

A photograph of the Aurora Borealis (Northern Lights) over a snowy, rocky landscape. The aurora displays vibrant green and yellow-green curtains of light against a dark, star-filled night sky. The foreground shows snow-covered ground and dark rocks. A teal-colored banner with a wavy edge is positioned at the bottom, containing the text.

# **ENG 3165 LECTURE 13**

THERMODYNAMICS COMPONENT

# Heat Transfer





# Introduction

- ❑ This lecture concludes the Thermodynamics component of the ENG 3165 Course.
- ❑ It provides an overview of the three main heat transfer methods; mainly **Conduction**, **Convection** and **Radiation**.

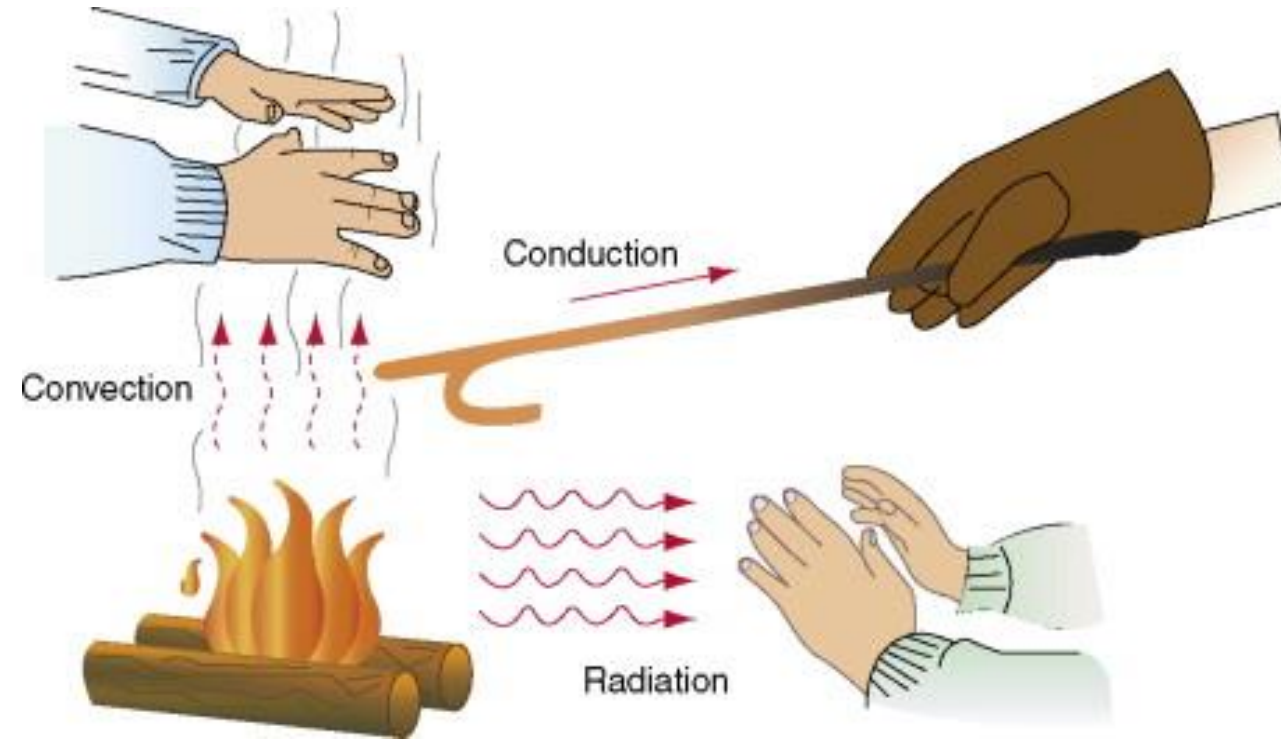
# GENERAL INTRODUCTION

- So far we have discussed different thermodynamic states and observed the property changes and from this deduced the heat transfer.
- Heat flow is transient problem so its analysis will involve more than investigation of equilibrium states.
- The laws of heat transfer obey the first and second laws of thermodynamics; energy is conserved and heat must flow from hot to cold.
- The transfer of heat can take place by two phenomena known as **conduction** and **radiation**. These phenomena may take place in a given system on their own or they may occur simultaneously. As the result of conduction and for radiation occurring into a fluid media then a transport transfer of heat may occur called **convection**.

# GENERAL INTRODUCTION

## Heat Transfer

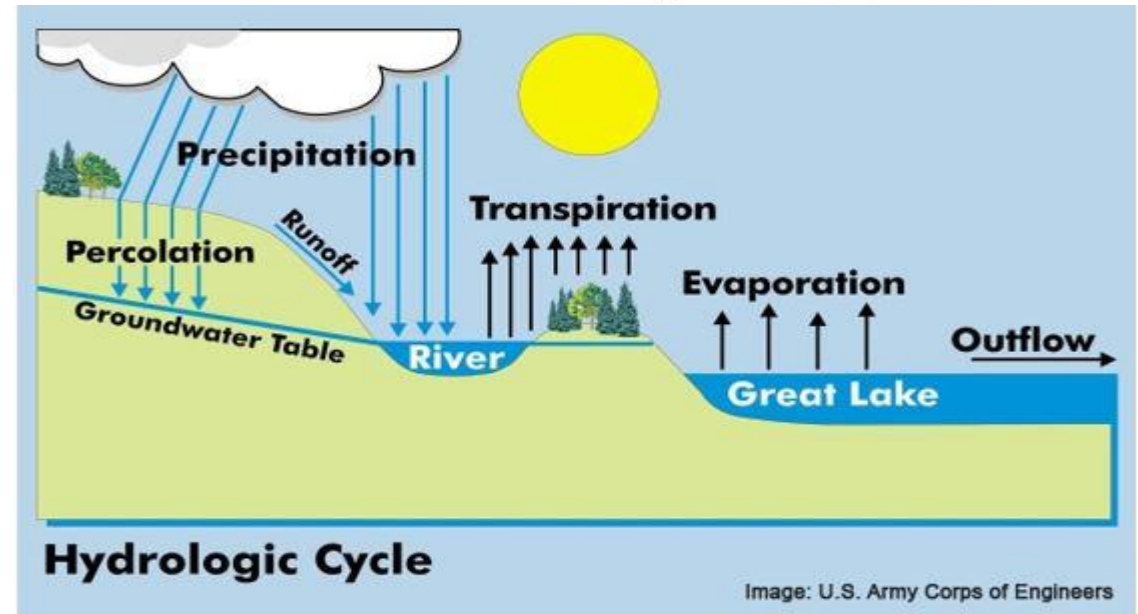
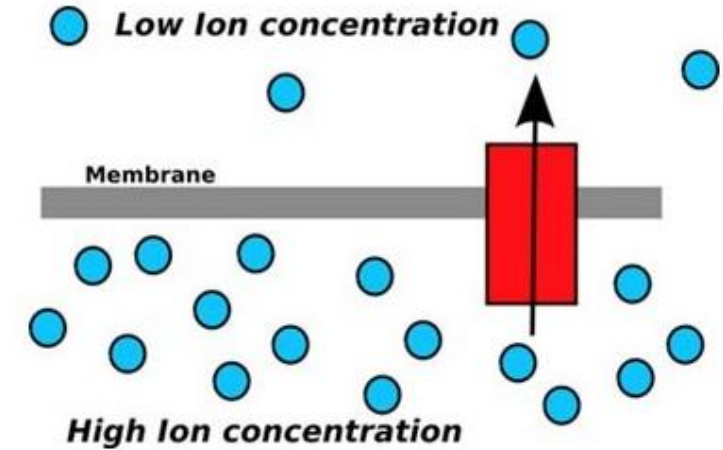
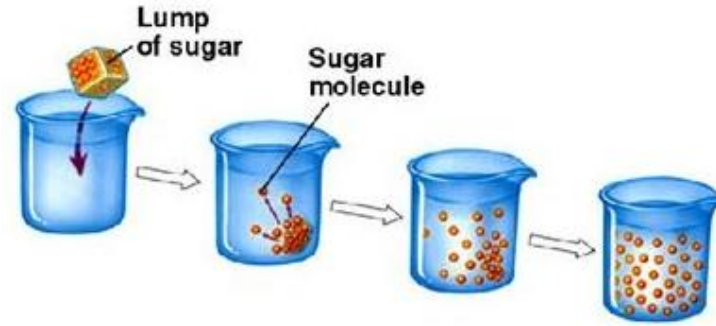
- Heat transfer is flow of energy solely due to a temperature difference or gradient
- From the Second Law of Thermodynamics, heat flows in the direction of decreasing temperature – down a temperature gradient.
- Heat energy can be transported through a solid, liquid, gas or even a vacuum.



# GENERAL INTRODUCTION

## Mass Transfer

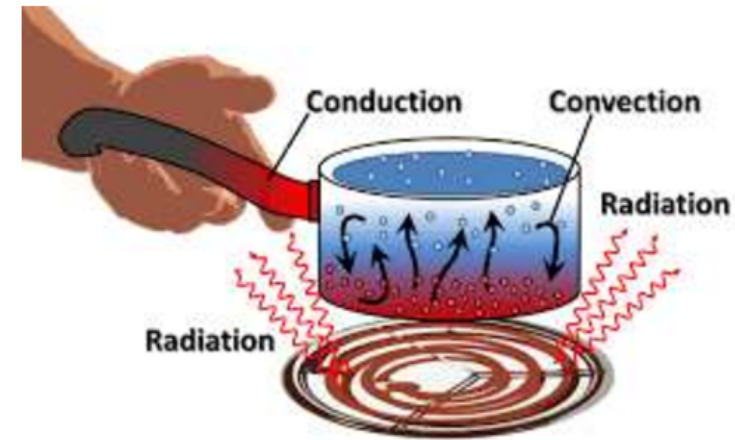
- Mass transfer is the **net movement of mass** from one location, usually meaning stream, phase, fraction or component, to another.
- This is most commonly from the region of high concentration to the lower concentration. An example is the evaporation of water from a pond to the atmosphere.



# CONDUCTION

A. **Conduction:** The transfer of energy from the **more energetic particles** of a substance to the adjacent **less energetic** ones as a result of interactions between the **particles**.

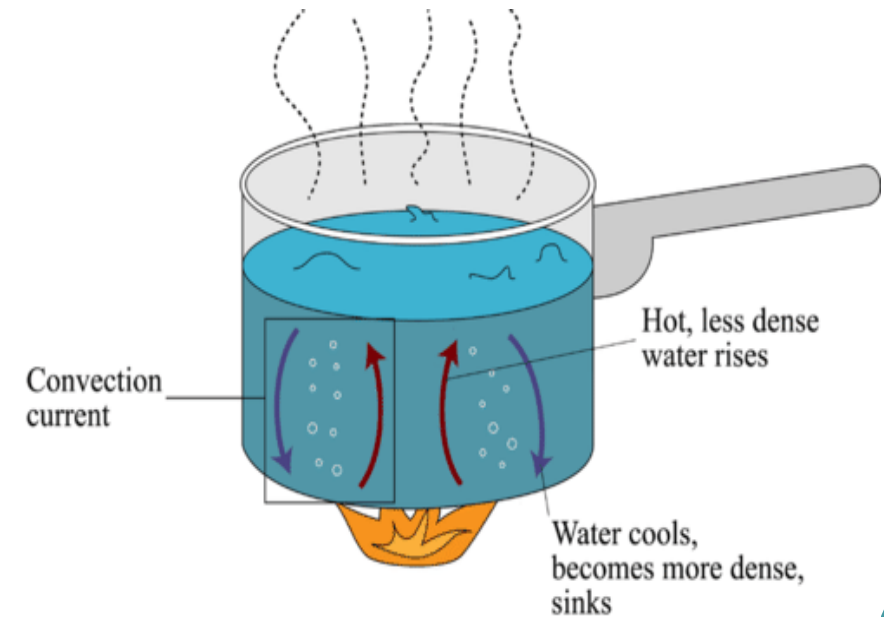
- In **solids**, it is due to the combination of *vibrations* of the molecules in a lattice and the energy transport by *free electrons* (i.e. *solids in metallic form*).
- In **gases and liquids**, conduction is due to the *collisions* and *diffusion* of the molecules during their random motion.



# CONVECTION

B. **Convection**: Thermal convection is the process by which heat transfer occurs via bulk motion or currents of moving **fluid**.

- Heat is transferred through molecular collisions between the fluid molecules.
- As a result of these collisions, the temperature in the fluid changes, the density varies, and the bulk fluid motion occurs. The high- and low-temperature fluid elements mix, and heat is transferred through convection.





# RADIATION

**C. Radiation:** The energy emitted by matter in the form of *electromagnetic waves* (or *photons*) as a result of the changes in the *electronic configurations of the atoms or molecules*.

- Unlike conduction and convection, the transfer of heat by radiation does not require the presence of an *intervening medium*.
- In fact, heat transfer by **radiation is fastest** (at the speed of light) and it suffers no attenuation in a vacuum.
- This is how the energy of the sun reaches the earth.



# LAWS OF HEAT TRANSFER

$$q = h\Delta T$$

where

$q$  is the local heat flux density [ $\text{W.m}^{-2}$ ]

$h$  is the heat transfer coefficient [ $\text{W.m}^{-2}.\text{K}$ ]

$\Delta T$  is the temperature difference [K]

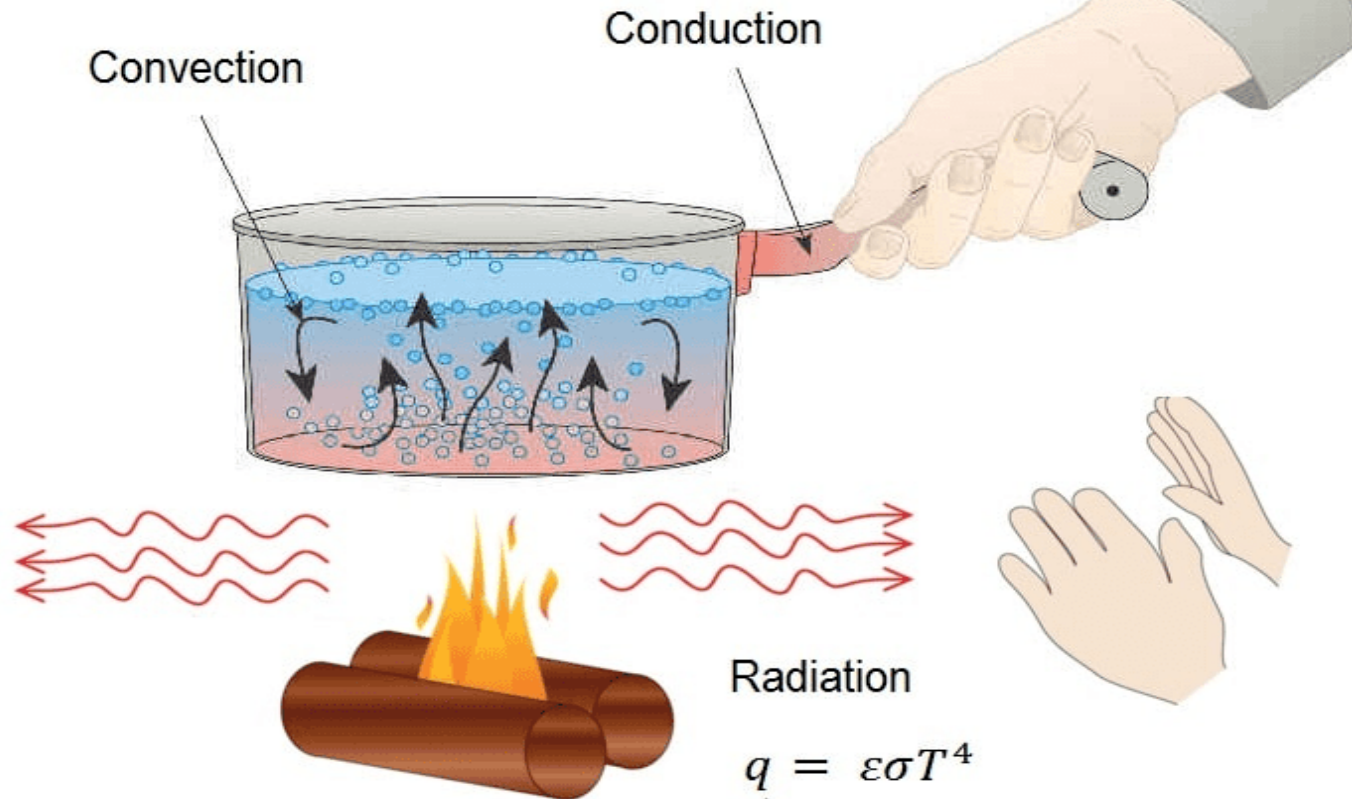
$$q = -k\nabla T$$

where

$q$  is the local heat flux density [ $\text{W.m}^{-2}$ ]

$k$  is the materials conductivity [ $\text{W.m}^{-1}.\text{K}^{-1}$ ]

$\nabla T$  is the temperature gradient [ $\text{K.m}^{-1}$ ]



Radiation

$$q = \varepsilon\sigma T^4$$

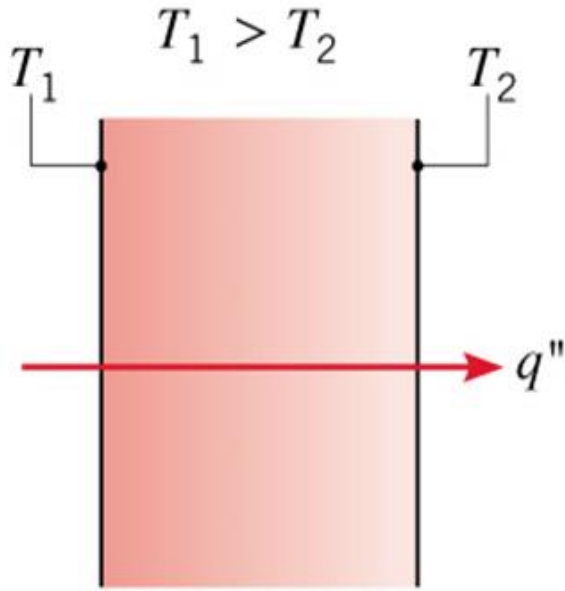
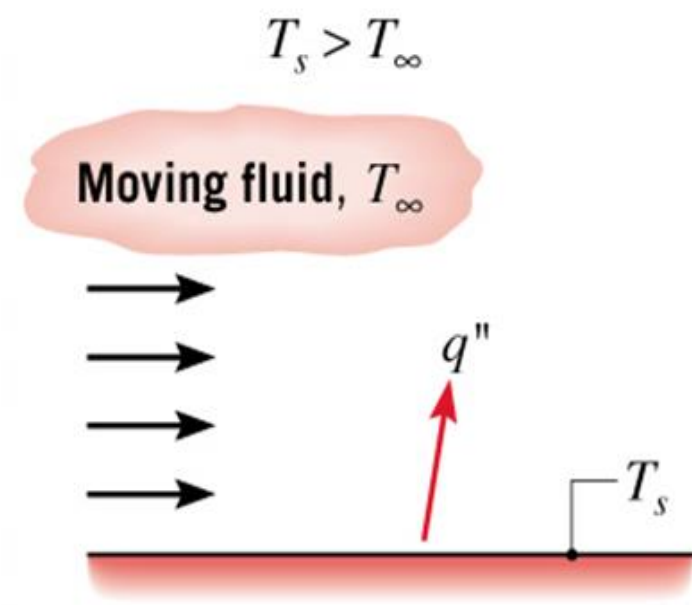
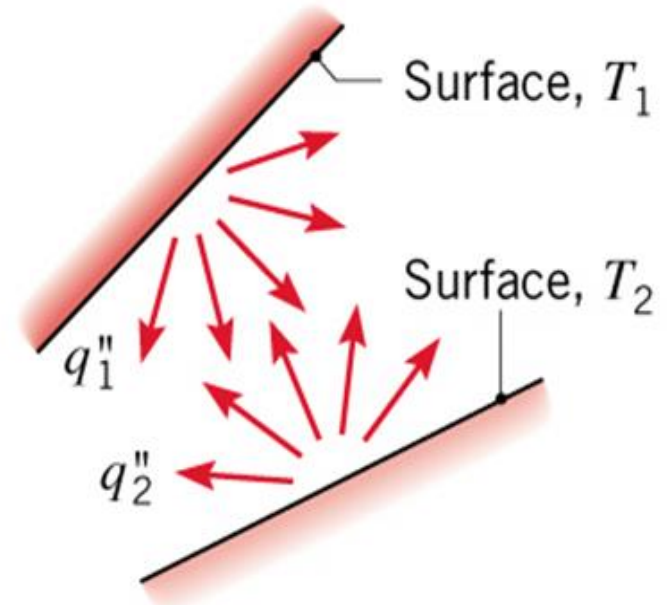
where

$q$  is the power radiated from an object [ $\text{W.m}^{-2}$ ]

$\sigma$  is the Stefan-Boltzmann constant [ $\text{W.m}^{-2}.\text{K}^{-4}$ ]

$\varepsilon$  is the emissivity of the surface of a material [-]

# LAWS OF HEAT TRANSFER

Conduction through a solid or a stationary fluid	Convection from a surface to a moving fluid	Net radiation heat exchange between two surfaces
 <p>A diagram showing a rectangular solid block with a red-to-white gradient. The left face is at temperature <math>T_1</math> and the right face is at temperature <math>T_2</math>, with <math>T_1 &gt; T_2</math> indicated above the block. A red arrow labeled <math>q''</math> points from the left face to the right face, representing the heat flux.</p>	 <p>A diagram showing a horizontal surface at temperature <math>T_s</math>. Above the surface is a cloud labeled "Moving fluid, <math>T_\infty</math>". The condition <math>T_s &gt; T_\infty</math> is written above the cloud. Four black arrows point from the surface towards the fluid, and a red arrow labeled <math>q''</math> points upwards from the surface, representing the convective heat flux.</p>	 <p>A diagram showing two surfaces, "Surface, <math>T_1</math>" (top) and "Surface, <math>T_2</math>" (bottom). Red arrows represent radiation. Arrows labeled <math>q_1''</math> point from Surface 1 towards Surface 2. Arrows labeled <math>q_2''</math> point from Surface 2 towards Surface 1. Other red arrows point away from both surfaces, representing radiation to the surroundings.</p>

# LAWS OF HEAT TRANSFER

## CONDUCTION: FOURIER'S LAW

The rate of **heat conduction** through a plane layer is **proportional** to the **temperature difference across the layer** and the **heat transfer area**, but is **inversely proportional** to the **thickness** of the layer.

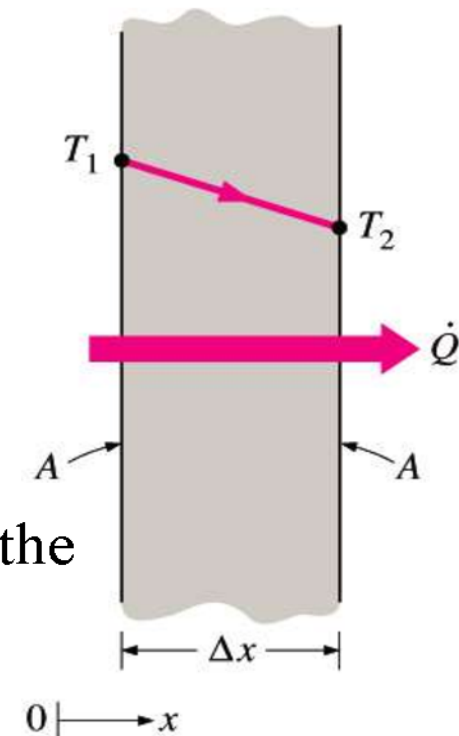
$$\text{Rate of heat conduction} \propto \frac{(\text{Area})(\text{Temperature difference})}{\text{Thickness}}$$

$$\dot{Q}_{\text{cond}} = kA \frac{T_1 - T_2}{\Delta x} = -kA \frac{\Delta T}{\Delta x} \quad (\text{W})$$

Where:-

**$K$  = Thermal conductivity**, : A measure of the ability of a material to conduct heat.

**$dT/dx$  = Temperature gradient** : The slope of the temperature curve on a  $T$ - $x$  diagram.





# LAWS OF HEAT TRANSFER

## CONDUCTION: FOURIER'S LAW

Material	Thermal conductivity $k$ (W.m <sup>-1</sup> .K <sup>-1</sup> )
Diamond	2450
Cu	385
Al	205
Brick	0.2
Glass	0.8
Body fat	0.2
Water	0.6
Wood	0.2
Styrofoam	0.01
Air	0.024

Thermal conductivity,  $k$   
property of the material

$k_{\text{diamond}}$  very high: perfect heat sink, e.g. for high power laser diodes

$k_{\text{human}}$  low: core temp relatively constant (37°C)

$k_{\text{air}}$  very low: good insulator  
\* home insulation  
\* woolen clothing  
\* windows double glazing

i.e, Metals – good conductors: electrons transfer energy from hot to cold

# LAWS OF HEAT TRANSFER

## CONDUCTION: FOURIER'S LAW

### THERMAL DIFFUSIVITY

- In heat transfer analysis, the **ratio of the thermal conductivity to the heat capacity** is an important property termed the *thermal diffusivity*  $\alpha$ , which is

$$\alpha = \frac{k}{\rho c_p} \quad m^2/s.$$

This value describes how quickly a material reacts to a change in temperature.

**Proof its SI units and what is the similar property in fluid flow?**

- It measures the ability of a material to **conduct thermal energy** relative to its ability to **store thermal energy**.
- So what does it mean when materials have **large** and **small** value of  $\alpha$ ?
- For a large  $\alpha$  will respond **quickly** to changes in their thermal environment, and ,For a small  $\alpha$  will respond more **sluggishly**, taking longer to reach a new equilibrium condition.  
Example: **WAX**
- In order to predict cooling processes or to simulate temperature fields, the thermal diffusivity must be known; it is a requisite for solving the **Fourier Differential Equation** for unsteady heat conduction.

# Example

A brick wall 250 mm thick is faced with concrete 50 mm thick. The brick has a coefficient of thermal conductivity of 0.69 W/m K while that of the concrete is 0.93 W/m K. If the temperature of the exposed brick face is 30°C and that of the concrete is 5°C, determine the heat lost/h through a wall 10 m long and 5 m high. Determine, also, the interface temperature.

$$\begin{aligned}\dot{Q} &= \frac{A(t_1 - t_2)}{x_1/k_1 + x_2/k_2} = \frac{(10 \times 5) \times (30 - 5)}{0.25/0.69 + 0.05/0.93} \\ &= \frac{50 \times 25}{0.362 + 0.054} = \frac{1250}{0.416} = \underline{3005 \text{ W}} = \underline{3005 \text{ J/s}} \\ &= \underline{3.005 \text{ kJ/s}}\end{aligned}$$

$$\therefore \text{Heat lost/h} = 3 \times 3600 = \underline{10800 \text{ kJ}}$$

# Example

For the brick wall,

$$\dot{Q} = \frac{k_1 A (t_1 - t_2)}{x_1}$$

$$\begin{aligned}\therefore t_2 &= t_1 - \frac{\dot{Q} x_1}{k_1 A} = 30 - \frac{3000 \times 0.25}{0.69 \times 50} \\ &= 30 - 21.7 = 8.3^\circ\text{C} = \text{interface temperature}\end{aligned}$$

Alternatively, for the concrete,

$$\dot{Q} = \frac{k_2 A (t_2 - t_3)}{x_2}$$

$$\begin{aligned}\therefore t_2 &= t_3 + \frac{\dot{Q} x_2}{k_2 A} = 5 + \frac{3000 \times 0.05}{0.93 \times 50} \\ &= 5 + 3.3 = \underline{8.3^\circ\text{C}}\end{aligned}$$



# LAWS OF HEAT TRANSFER

## CONVECTION: NEWTON'S LAW OF COOLING

### Newton's law of cooling

$$\dot{Q}_{\text{conv}} = hA_s (T_s - T_{\infty}) \quad (\text{W})$$

$h$	convection heat transfer coefficient, $\text{W/m}^2 \cdot ^\circ\text{C}$
$A_s$	the surface area through which convection heat transfer takes place
$T_s$	the surface temperature
$T_{\infty}$	the temperature of the fluid sufficiently far from the surface

# LAWS OF HEAT TRANSFER

## RADIATION: STEFAN-BOLTZMANN LAW

- In heat transfer studies we are interested in *thermal radiation*, which is the form of radiation emitted by bodies because of their temperature.
- All bodies at a temperature above absolute zero emit thermal radiation.

### Absorption & Stefan-Boltzmann Law

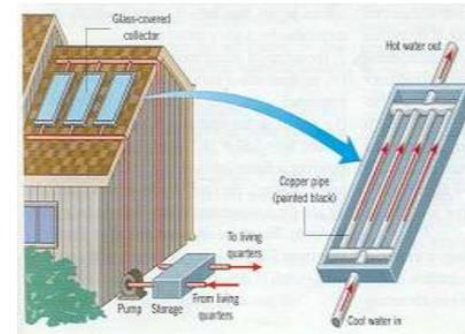
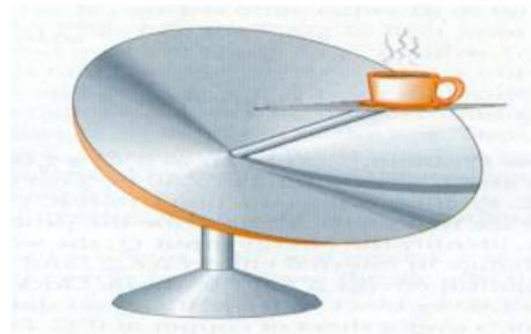
$$\dot{Q}_{\text{emit, max}} = \sigma A_s T_s^4 \quad (\text{W})$$

Stefan-Boltzmann law

Where:-

- Surface Area,  $A$
- Stefan-Boltzmann constant,  $\sigma = 5.67 \times 10^{-8} \text{ W.m}^{-2}.\text{K}^{-4}$

### Applications on radiation heat transfer



**“Is not fire a body heated so hot as to emit light copiously? For what as is a red hot iron than fire? And what else is a burning hot coal than red hot wood?”**

Isaac Newton



# Thank You

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