

R. W. HAYWOOD

Thermodynamic Tables in SI (metric) Units

(Système International d'Unités)

WITH CONVERSION FACTORS TO
OTHER METRIC AND BRITISH UNITS
AND

ENTHALPY-ENTROPY DIAGRAM FOR
STEAM
PRESSURE-ENTHALPY DIAGRAM FOR
REFRIGERANT-12

THIRD EDITION

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THERMODYNAMIC TABLES
IN
SI (METRIC) UNITS

(SYSTÈME INTERNATIONAL D'UNITÉS)

WITH CONVERSION FACTORS TO
OTHER METRIC AND BRITISH UNITS

R. W. HAYWOOD

*Emeritus Reader in Engineering Thermodynamics
University of Cambridge*

THIRD EDITION



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**THERMODYNAMIC TABLES
IN SI (METRIC) UNITS**

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PREFACE

These Tables in SI (metric) units have been modelled on the author's earlier Tables in British units, but further individual tables have been introduced. The steam tables have been extended to higher pressures and have been computed from more recent formulae. The table giving the properties of semi-perfect gases provides data for the calculation of enthalpies in the First Law analysis of combustion processes, while the tables of equilibrium constants and standard enthalpies of reaction cater for the effects of dissociation at higher temperatures. The tables giving the properties of air at low temperatures enable problems involving liquefaction and refrigeration at cryogenic temperatures to be handled, while the tables of transport properties of various fluids provide data for the solution of problems in heat transfer.

The most difficult decision in the construction of these new Tables arose in relation to the unit of pressure to be used. The basic SI unit of pressure, the N/m^2 , is too small a unit for practical convenience in most engineering applications. As a result, the general tendency has been to favour the bar (10^5 N/m^2), which is about one atmosphere. However, 10^5 is not one of the recognised multiples of the *Système International*, which prefers steps of 10^3 , and the use of multiples and submultiples of the bar would be even more objectionable. A still more serious objection to the use of the bar is that this perpetuates the need for a unit conversion factor in energy conversion calculations. Even though this factor is a multiple of 10, its presence disturbs the simple coherence of the *Système International*, which results from the fact that $1 \text{ N} = 1 \text{ kg m/s}^2$ and $1 \text{ J} = 1 \text{ N m}$. In a set of Tables designed primarily for use in Universities and Technical Colleges, it was consequently considered to be educationally desirable that tabulation should be primarily in terms of the N/m^2 , and its recognised multiples; at the same time the corresponding number of bars has been indicated alongside each table at conveniently frequent intervals. In the saturation table for steam, it has been found convenient to change from the use of kN/m^2 to the use of MN/m^2 at about atmospheric pressure. In all other tables the pressure is quoted in MN/m^2 . All pressures listed are **absolute** pressures.

To users of the Tables unfamiliar with SI units, attention is drawn to the fact that the kilogram, not the gram, is the basic SI unit of mass, and it is in terms of this unit that the SI is a coherent system of units, since $1 \text{ N} = 1 \text{ kg m/s}^2$. It is not practicable to express 10^{-3} kilogram as a 'millikilogram', so that it is still described as a 'gram'. A similarly unsatisfactory situation exists in relation to the *kmol* and the *mol*. To counter this anomaly, a new name for the kilogram mass is clearly needed; the author has suggested *berg* (unit symbol b), but international agreement on any change of name is not likely to be achieved in a short time.

The terminology of that branch of science concerned with temperature has long been in a most unsatisfactory state, and two Appendices are devoted to this topic in order to make clear the usage adopted in the Tables, in which all temperatures listed are thermodynamic in definition. In these Appendices, no mention is made of scale temperatures on the International Practical Scales of Temperature defined in 1948 and 1960, since a redefinition of these scales in terms of the kelvin unit of thermodynamic temperature is likely to be made in

1968.* It seems that there may then be good hope of achieving a rational simplification of nomenclature and symbology which will greatly reduce the current confusions arising from the present multiplicity of symbols. The usage adopted in the Tables is believed to be close to that which will eventually result from such simplification.

The stimulus for the production of these Tables was provided by the decision of the United Kingdom to commence the transition from British units to metric units of the *Système International*. Initially, many users of the Tables will be familiar with British units and with some commonly used non-SI metric units, but will be unfamiliar with SI units; with the passage of time, this situation will be reversed, but for many years engineers and scientists will need to consult earlier publications quoting data in British units and in non-SI metric units. The Appendices giving definitions and conversion factors have been prepared with this situation in mind. The inclusion of exact conversion factors is instructive in revealing the definitive relationships between the different systems of units. Rounded values for slide-rule calculation have also been quoted, but digital computers are increasingly being used and, for exact calculations, it is illogical to feed into such computers a conversion factor that has been rounded to the number of significant figures adequate only for slide-rule calculation. It would, of course, also be illogical to use exact conversion factors when such accuracy was not warranted. Throughout these Tables, exact numerical values are printed in **bold** type.

The author is especially grateful to all those on whose work he has drawn in compiling the Tables. He is also indebted to his colleagues for helpful advice in planning the initial lay-out of the Tables, to Dr J. H. Matthewman for programming the equations from which the property values for water substance and for Refrigerant-12 were computed and to Mr P. K. Clarkson for computational assistance in the preparation of various tables. Dr Matthewman and the author have prepared an enthalpy-entropy diagram for steam and a pressure-enthalpy diagram for Refrigerant-12; these were drawn by digital plotter from the same equations as those used in calculating the values for the respective tables and are available for use with the Tables.

R. W. HAYWOOD

Cambridge

* *The Rational Treatment of Temperature and Temperature Scales*, Haywood, R. W., *Proc. I. Mech. E.*, 1967-68, Volume 182, Part 1; contribution to the discussion by J. Terrien and J. de Boer. (This change was made in 1968. See *The International Practical Temperature Scale of 1968*, HMSO, London, 1969 and Amended Edition of 1975, HMSO, London, 1976.)

SECOND EDITION 1972

Tables 7, 9, 10, 11 and 12 have been extended. The treatment of the *mole* has been brought into line with current international usage and a number of minor corrections and additions have been made.

NOTE ON THE 1978 REPRINT

A table of SI prefixes has been added. A more complete statement relating to the standard enthalpy of reaction has been given at the head of Table 5. The quoted value of the molar number and the conversion factor for the UK gallon have been brought into line with a more recent evaluation and specification respectively. A typographical error in the previously quoted conversion factor for the US gallon has also been corrected.

These Tables and Diagrams are also now available in Spanish translation [Haywood, R. W., *Tablas Termodinámica en Unidades SI (métricas)*. Trans. by A. E. Estrada, Compañía Editorial Continental, S.A., Mexico (1977).]

PREFACE TO THE THIRD EDITION 1990

In this third edition, the only major change is in the presentation of Equilibrium Constants in Table 4, in order to bring this into line with more generally accepted current practice. The change which most greatly affects the tabulated values is that they are presented in terms of the natural logarithms of the equilibrium constants, instead of logarithms to the base 10. A much smaller change in the tabulated values arises from the fact that partial pressures have been expressed in terms of the bar (1 bar = 0.1 MN/m²), instead of the standard atmosphere (1 atm = 0.101325 MN/m²). A third change, which does not affect the numerical values, is that, in the formula for $\ln K_p$, these partial pressures are expressed non-dimensionally in terms of a quantity given the symbol $p^* \equiv p_i/p_0$, where p_i is the partial pressure of species i in bars, and p_0 is the *standard pressure* of 1 bar: thus p^* is numerically equal to p_i . This change in the standard pressure, from the previous value of 1 atm, is in line with the 1982 recommendation of the International Union of Pure and Applied Chemistry (IUPAC). The expression of partial pressures non-dimensionally ensures dimensional consistency in the formula for $\ln K_p$, since logarithms are dimensionless numbers.

The values of $\ln (K_p)_{\text{bar}}$ listed in Table 4 are everywhere numerically consistent with the values of $\log_{10} (K_p)_{\text{atm}}$ given in Table 4 of the second edition, and a simple formula is given by which values of the latter can readily be calculated from the tabulated values of the former.

On page 2, the quoted value of the molar (universal) gas constant $\bar{R}$ has been increased by 2 in the last figure, in line with the latest internationally accepted value. That change is of no practical engineering significance.

In Appendix A, the previous formal definitions of the *candela* and the *metre* have been replaced by the new definitions promulgated respectively by the 16th CGPM, 1979, and the 17th CGPM, 1983.

I have to thank my former colleague in the University Engineering Department at Cambridge, Dr J. D. Lewins, for his suggestions on the updating of these Tables, and for kindly providing me with copy of some material to which I no longer had access.

R. W. HAYWOOD

With respect to the asterisked note on page viii, the *International Temperature Scale of 1990*, ITS-90, has superseded the International Practical Temperature Scale of 1968/75. Information on the definition of ITS-90 is available from the Division of Quantum Metrology, National Physical Laboratory, Teddington, Middlesex.

GENERAL DATA

Precise data relating to temperature, definitions of units and unit conversion factors are given in the Appendices.

Temperature: At a *temperature* (thermodynamic) of T kelvins (namely T K), the corresponding truncated thermodynamic temperature called the *Celsius temperature* is t Celsius, written symbolically as t °C, where:

$$t = T - 273.15.$$

The difference in temperature between t_1 Celsius (t_1 °C) and t_2 Celsius (t_2 °C) is thus $(t_1 - t_2)$ kelvins, namely $(t_1 - t_2)$ K.

Note: Thermodynamic temperatures expressed in kelvins are commonly described as *absolute* temperatures.

Pressure:

$$1 \text{ bar} = 10^5 \text{ N/m}^2.$$

$$1 \text{ atm} = 1.01325 \text{ bar} = 0.101325 \text{ MN/m}^2 \\ = 760 \text{ torr} \approx 760 \text{ mmHg to 1 part in 7 million.}$$

(For the definition of the mmHg, see Appendix D.)

Standard temperature and pressure (s.t.p.): 0 °C and 1 bar (formerly 1 atm).

Unified atomic mass unit ($\frac{1}{12}$ of an atom of the nuclide ^{12}C): 1.66054×10^{-27} kg.

Atomic weights: Hydrogen 1*, Helium 4, Carbon 12, Nitrogen 14, Oxygen 16, Sulphur 32, Argon 40.

Mole: A *mole* (mol) is a unit of *quantity of particles of specified kind*; it is not a unit of mass. Its formal definition is given in Appendix A.

Molar mass: The *molar mass* is the mass in grams (kilograms) of a mole (kilomole) of the specified substance.

Molar number (Avogadro constant): 6.022×10^{23} particles/mol ($\equiv 6.022 \times 10^{26}$ particles/kmol).

Electron charge: 1.60×10^{-19} coulomb.

Stefan-Boltzmann constant: $5.67 \times 10^{-8} \text{ W/m}^2 \text{ K}^4$.

* A more exact value is 1.008.

TABLE 1. CALORIFIC VALUES

In this Table, the *calorific value* is the enthalpy decrease on combustion when the reactants and products are at 25 °C. In the evaluation of the lower calorific value the steam is taken as being dry saturated.

Substance	Molar mass kg/kmol	B.P. at 1 atm °C	Phase	Calorific value kJ/kg	
C	{ to CO to CO ₂	-191.5	sol.	9 190	
				32 760	
	CO		gas	10 100	
				Higher (gross) (H ₂ O to water)	Lower (net) (H ₂ O to steam)
H ₂	2*	-252.9	gas	142 000	120 000
CH ₄ (methane)	16	-161.5	gas	55 500	50 010
C ₂ H ₆ (ethane)	30	-88.5	gas	51 870	47 470
C ₃ H ₆ (propylene)	42	-47.7	gas	48 940	45 800
C ₃ H ₈ (propane)	44	-42.1	gas	50 360	46 360
C ₄ H ₁₀ (butane)	58	-0.5	gas	49 520	45 730
C ₈ H ₁₈ (n-octane)	114	125.7	gas	48 270	44 800
			liq.	47 900	44 430

* A more exact value is 2.016.

PERFECT GASES

At normal atmospheric conditions, and over a limited range of temperature and pressure, the gases listed in Table 2 may be assumed to behave as perfect gases. That is, they may be assumed to have the equation of state $pv = RT$, and to have constant specific heat capacities.

Molar (universal) gas constant: $R = MR = 8.3145 \text{ kJ/kmol K}$.

Molar volume of a perfect gas: 1 kmol of any perfect gas occupies a volume of approximately 22.4 m³ at s.t.p. (0 °C and 1 bar).

TABLE 2

Gas	Molar mass kg/kmol	Gas constant kJ/kg K	Specific heat capacity kJ/kg K		c_p/c_v
			c_p	c_v	
Air	29.0	0.287	1.01	0.72	1.40
Atmospheric nitrogen †	28.15	0.295	1.03	0.74	1.40
N ₂	28	0.297	1.04	0.74	1.40
O ₂	32	0.260	0.92	0.66	1.40
A	40	0.208	0.52	0.31	1.67
H ₂	2*	4.12	14.20	10.08	1.41
He	4	2.08	5.19	3.11	1.67
CO	28	0.297	1.04	0.74	1.40
CO ₂	44	0.189	0.82	0.63	1.31
SO ₂	64	0.130	0.61	0.48	1.26
CH ₄	16	0.520	2.23	1.71	1.31
C ₂ H ₆	30	0.277	1.75	1.47	1.19
C ₃ H ₈	42	0.198	1.52	1.32	1.15

* A more exact value is 2.016.

† Air contains 0.93 % of argon (A) and traces of other gases; these and the nitrogen together are called *atmospheric nitrogen*.

Real gases are not perfect gases, and the rounded values for R , c_p , c_v and c_p/c_v listed above do not exactly satisfy the relationships between these quantities that would obtain for perfect gases.

Air composition:

Volumetric (and molar): 21.0 % O₂, 79.0 % atmospheric nitrogen.

Gravimetric: 23.2 % O₂, 76.8 % atmospheric nitrogen.

SEMI-PERFECT GASES

At low pressures, and over the temperature range quoted, the gases listed in this Table behave as semi-perfect gases. That is, while having the molar equation of state $p\bar{v} = \bar{R}T$, their specific heat capacities are variable but are functions only of temperature.

TABLE 3. MOLAR ENTHALPIES AT LOW PRESSURES

Warning: This table lists *absolute* temperatures.

Gas ...	Air	N ₂	O ₂	H ₂	CO	CO ₂	H ₂ O	
Molar mass ...	29	28	32	2*	28	44	18	
kg/kmol ...								
Temperature K	Molar enthalpy MJ/kmol							Temperature K
200	5.79	5.81	5.79	5.69	5.81	5.96	6.62	200
25 °C 298.15	8.64	8.67	8.66	8.46	8.67	9.37	9.90	298.15 25 °C
300	8.70	8.72	8.71	8.52	8.72	9.44	9.96	300
400	11.62	11.64	11.68	11.42	11.64	13.37	13.35	400
500	14.57	14.58	14.74	14.34	14.60	17.67	16.82	500
600	17.59	17.56	17.90	17.27	17.61	22.27	20.39	600
700	20.66	20.61	21.16	20.21	20.69	27.12	24.09	700
800	23.81	23.72	24.50	23.16	23.85	32.18	27.90	800
900	27.03	26.89	27.90	26.13	27.07	37.41	31.83	900
1000	30.30	30.14	31.37	29.14	30.36	42.78	35.90	1000
1100	33.64	33.44	34.88	32.18	33.71	48.27	40.09	1100
1200	37.02	36.79	38.43	35.26	37.11	53.87	44.41	1200
1300	40.44	40.19	42.01	38.38	40.54	59.55	48.84	1300
1400	43.90	43.62	45.63	41.54	44.02	65.31	53.39	1400
1500	47.39	47.09	49.27	44.75	47.53	71.13	58.05	1500
1600	50.92	50.59	52.94	48.00	51.07	77.01	62.81	1600
1700	54.47	54.12	56.63	51.29	54.63	82.94	67.65	1700
1800	58.04	57.67	60.35	54.62	58.21	88.92	72.58	1800
1900	61.63	61.25	64.09	58.00	61.81	94.93	77.59	1900
2000	65.24	64.84	67.86	61.40	65.42	100.97	82.67	2000
2100	68.87	68.44	71.65	64.84	69.06	107.05	87.81	2100
2200	72.52	72.06	75.46	68.31	72.70	113.15	93.01	2200
2300	76.18	75.70	79.29	71.82	76.36	119.28	98.27	2300
2400	79.86	79.35	83.14	75.35	80.03	125.43	103.58	2400
2500	83.55	83.01	87.02	78.90	83.71	131.61	108.94	2500
2600	87.25	86.68	90.92	82.48	87.40	137.80	114.34	2600
2700	90.96	90.36	94.83	86.09	91.10	144.02	119.78	2700
2800	94.69	94.05	98.77	89.72	94.80	150.25	125.26	2800
2900	98.42	97.74	102.72	93.37	98.51	156.50	130.77	2900
3000	102.16	101.44	106.70	97.04	102.23	162.76	136.31	3000

* A more exact value is 2.016.

Note: (1) The molar enthalpies listed are those in the ideal gas state at zero pressure, but the values given are also valid at and around atmospheric pressure.

(2) In this table, the arbitrary datum state for zero enthalpy is that of the substance in the ideal gas state at zero pressure and zero absolute temperature. (Warning: In Tables 6-12, the arbitrary datum state for H₂O is that of the saturated liquid at the triple point, at which state the internal energy and entropy are taken to be zero.)

(3) The values for atmospheric nitrogen, N₂*, may be taken to be the same as those for N₂.

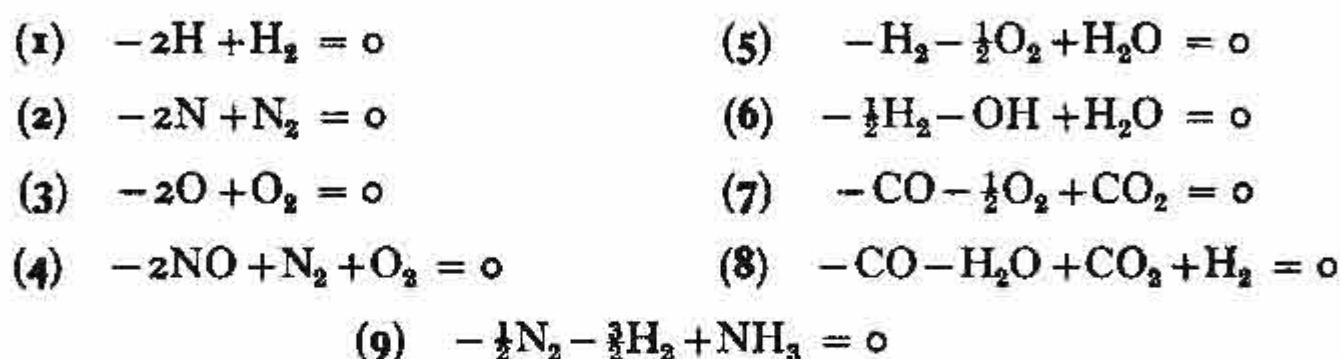
THERMOCHEMICAL DATA FOR EQUILIBRIUM REACTIONS

TABLES 4 AND 5 RELATE TO THE REACTIONS LISTED BELOW

STOICHIOMETRIC EQUATIONS

$$\sum_i \nu_i A_i = 0,$$

where ν_i is the *stoichiometric coefficient* of the substance whose *chemical symbol* is A_i .



EQUILIBRIUM CONSTANTS

$$\ln (K_p)_{\text{bar}} = \sum_i \nu_i \ln p_i^*$$

where $p_i^* \equiv p_i'/p_0$

p_i' $\equiv$ partial pressure of species A_i , in **bars**

$p_0 \equiv$ standard pressure $\equiv$ **1 bar**.

Thus p_i^* is numerically equal to p_i' , but is **dimensionless**. In the second edition of these Tables, p_i' was expressed in **atmospheres**, where $1 \text{ atm} \equiv 1.01325 \text{ bar}$ and $1 \text{ bar} \equiv 0.1 \text{ MN/m}^2$. The numerical relationship between the value of K_p as defined above, namely $(K_p)_{\text{bar}}$, and the value of K_p as previously defined, namely $(K_p)_{\text{atm}}$, is thus:

$$\ln (K_p)_{\text{bar}} = \ln (K_p)_{\text{atm}} + \sum_i \nu_i \ln 1.01325$$

The values of $\ln (K_p)_{\text{bar}}$ in Table 4 are everywhere consistent with the values of $\log_{10} (K_p)_{\text{atm}}$ given in Table 4 of the second edition, the two being related by the following expression:

$$\log_{10} (K_p)_{\text{atm}} = 0.434295 \ln (K_p)_{\text{bar}} - 0.00572 \sum_i \nu_i$$

TABLE 4. EQUILIBRIUM CONSTANTS

Warning: This table lists *absolute* temperatures.

Reaction number										
Temp. K	1 $\sum_i \nu_i$ = -1	2 $\sum_i \nu_i$ = -1	3 $\sum_i \nu_i$ = -1	4 $\sum_i \nu_i$ = 0	5 $\sum_i \nu_i$ = - $\frac{1}{2}$	6 $\sum_i \nu_i$ = - $\frac{1}{2}$	7 $\sum_i \nu_i$ = - $\frac{1}{2}$	8 $\sum_i \nu_i$ = 0	9 $\sum_i \nu_i$ = -1	Temp. K
$\ln(K_p)_{\text{bar}}$										
200	250.149	554.472	285.471	105.592	139.972	161.789	159.692	19.719	15.433	200
298	163.986	367.479	186.975	69.865	92.207	106.228	103.762	11.554	6.593	298
400	119.150	270.329	135.715	51.311	67.321	77.284	74.669	7.348	1.778	400
600	75.217	175.356	85.523	33.203	42.897	48.905	46.245	3.348	-3.191	600
800	53.126	127.753	60.319	24.145	30.592	34.634	32.036	1.444	-5.822	800
1000	39.803	99.127	45.150	18.706	23.162	26.033	23.528	0.366	-7.457	1000
1200	30.874	80.011	35.005	15.082	18.182	20.281	17.871	-0.311	-8.570	1200
1400	24.463	66.329	27.742	12.489	14.608	16.160	13.841	-0.767	-9.371	1400
1600	19.632	56.055	22.285	10.546	11.921	13.065	10.829	-1.091	-9.972	1600
1800	15.865	48.051	18.030	9.035	9.825	10.657	8.497	-1.329	-10.439	1800
2000	12.835	41.645	14.622	7.824	8.145	8.727	6.634	-1.510	-10.810	2000
2200	10.353	36.391	11.827	6.834	6.768	7.148	5.119	-1.649	-11.109	2200
2400	8.276	32.011	9.497	6.010	5.619	5.831	3.859	-1.759	-11.358	2400
2600	6.512	28.304	7.521	5.314	4.647	4.718	2.800	-1.847	-11.563	2600
2800	5.002	25.117	5.286	4.720	3.811	3.763	1.893	-1.918	-11.738	2800
3000	3.685	22.359	4.357	4.205	3.086	2.936	1.110	-1.976	-11.885	3000
3200	2.533	19.936	3.072	3.753	2.450	2.211	0.429	-2.022	-12.012	3200
3400	1.516	17.800	1.935	3.357	1.891	1.575	-0.170	-2.061	-12.122	3400
3600	0.609	15.898	0.926	3.007	1.391	1.007	-0.702	-2.093	-12.217	3600
3800	-0.207	14.198	0.019	2.694	0.944	0.500	-1.176	-2.121	-12.300	3800
4000	-0.939	12.660	-0.796	2.413	0.541	0.044	-1.600	-2.141	-12.373	4000
4500	-2.486	9.414	-2.514	1.828	-0.313	-0.921	-2.491	-2.178	-12.519	4500
5000	-3.725	6.807	-3.895	1.363	-0.997	-1.690	-3.178	-2.201	-12.624	5000
5500	-4.743	4.666	-5.024	0.986	-1.561	-2.318	-3.771	-2.210	-12.703	5500
6000	-5.590	2.865	-5.963	0.677	-2.033	-2.843	-4.246	-2.213	-12.760	6000

STANDARD FREE ENTHALPY OF REACTION

At a given temperature, the standard free enthalpy of reaction ΔG_T^0 (or *standard Gibbs function change*) may be calculated from the listed value of $\ln(K_p)_{\text{bar}}$ by the following equation:

$$\begin{aligned}\Delta G_T^0 &= -\bar{R}T \ln K_p \\ &= -8.3145 T \ln (K_p)_{\text{bar}}.\end{aligned}$$

STANDARD ENTHALPY OF REACTION

$$\Delta H_T^0 = \sum_i \nu_i [\tilde{h}_i]_T^0 = \sum_i \nu_i ([\Delta H_f]_T^0)_i$$

$$\text{where } [\tilde{h}_i]_T^0 = ([\Delta H_f]_{298}^0)_i + ([\bar{h}]_T^0 - [\bar{h}]_{298}^0)_i$$

and $([\Delta H_f]_T^0)_i$ is the *standard enthalpy of formation* of species i at temperature T (and a pressure $p_0 = 1$ bar).

TABLE 5. STANDARD ENTHALPY OF REACTION

Warning: This table lists *absolute* temperatures.

Reaction number										
Temp. K	1	2	3	4	5	6	7	8	9	Temp K
	$\Delta H_f^0/\text{MJ}$									
200	-434.7	-944.1	-496.9	-180.4	-240.9	-280.2	-282.1	-41.21	-43.71	200
298	-436.0	-945.3	-498.4	-180.6	-241.8	-281.3	-283.0	-41.17	-45.90	298
400	-437.3	-946.6	-499.8	-180.7	-242.8	-282.4	-283.5	-40.63	-48.04	400
600	-439.7	-948.9	-502.1	-180.7	-244.8	-284.1	-283.6	-38.88	-51.39	600
800	-442.1	-951.1	-503.9	-180.8	-246.5	-285.5	-283.3	-36.82	-53.66	800
1000	-444.5	-953.0	-505.4	-180.9	-247.9	-286.6	-282.6	-34.74	-55.07	1000
1200	-446.7	-954.7	-506.7	-180.9	-249.0	-287.4	-281.8	-32.79	-55.83	1200
1400	-448.7	-956.1	-507.8	-181.0	-249.9	-287.9	-280.9	-30.98	-56.07	1400
1600	-450.6	-957.5	-508.9	-181.0	-250.6	-288.4	-279.9	-29.29	-55.99	1600
1800	-452.3	-958.7	-509.8	-181.0	-251.2	-288.6	-278.9	-27.71	-55.66	1800
2000	-453.8	-959.9	-510.6	-181.0	-251.7	-288.8	-277.9	-26.22	-55.19	2000
2200	-455.2	-961.0	-511.4	-180.8	-252.1	-288.9	-276.8	-24.79	-54.61	2200
2400	-456.4	-962.1	-512.0	-180.7	-252.4	-289.0	-275.8	-23.41	-53.92	2400
2600	-457.6	-963.1	-512.5	-180.4	-252.7	-289.0	-274.8	-22.07	-53.12	2600
2800	-458.6	-964.1	-513.0	-180.1	-253.0	-288.9	-273.7	-20.77	-52.22	2800
3000	-459.6	-965.0	-513.4	-179.7	-253.3	-288.9	-272.7	-19.49	-51.20	3000
3200	-460.4	-966.0	-513.8	-179.3	-253.5	-288.8	-271.7	-18.19	-50.10	3200
3400	-461.2	-967.0	-514.1	-178.7	-253.8	-288.7	-270.7	-16.91	-48.94	3400
3600	-461.9	-968.1	-514.4	-178.2	-254.1	-288.6	-269.8	-15.62	-47.75	3600
3800	-462.5	-969.2	-514.6	-177.6	-254.5	-288.5	-268.8	-14.33	-46.49	3800
4000	-463.0	-970.4	-514.8	-176.9	-254.8	-288.4	-267.8	-13.00	-45.19	4000
4500	-464.0	-973.8	-515.3	-175.2	-255.9	-288.1	-265.5	-9.57	-41.68	4500
5000	-464.6	-977.9	-515.9	-173.2	-257.2	-288.0	-263.1	-5.95	-37.79	5000
5500	-464.8	-982.9	-516.5	-171.1	-258.6	-287.9	-260.7	-2.10	-33.56	5500
6000	-464.7	-989.0	-517.2	-169.0	-260.3	-287.9	-258.2	2.01	-28.98	6000

STEAM TABLES

In Tables 6–12, giving the thermodynamic properties of ordinary water substance, the arbitrary datum state for zero internal energy and entropy is that of the saturated liquid at the triple point, which is the state point at which the solid, liquid and vapour are together in equilibrium.

TABLE 6. TRIPLE POINT OF WATER

TEMPERATURE: **273.16 K**
 CELSIUS TEMPERATURE: **0.01 °C**
 PRESSURE: **0.6112 kN/m²**

Phase	Specific volume m ³ /kg	Specific enthalpy kJ/kg	Specific entropy kJ/kg K
Ice	1.0905×10^{-3}	-333.5	-1.221
Water	1.0002×10^{-3}	0.000 61	zero
Steam	206.2	2501.6	9.157

TABLE 7. SATURATED WATER AND STEAM
TEMPERATURES FROM THE TRIPLE POINT TO 100 °C

[100 kN/m ² = 1 bar ≈ 14.5 lbf/in ²]											
Celsius temp., °C <i>t</i>	Pressure kN/m ² <i>p</i>	Specific volume m ³ /kg		Specific internal energy kJ/kg		Specific enthalpy kJ/kg			Specific entropy kJ/kg K		Celsius temp., °C <i>t</i>
		Water <i>v_f</i>	Steam <i>v_g</i>	Water <i>u_f</i>	Steam <i>u_g</i>	Water <i>h_f</i>	Evaporation <i>h_{fg}</i>	Steam <i>h_g</i>	Water <i>s_f</i>	Steam <i>s_g</i>	
0.01	0.611	0.001000	206.2	zero	2375.6	+0.0	2501.6	2501.6	zero	9.157	0.01 Triple point
2	0.705	0.001000	179.9	8.4	2378.3	8.4	2496.8	2505.2	0.031	9.105	2
4	0.813	0.001000	157.3	16.8	2381.1	16.8	2492.1	2508.9	0.061	9.053	4
6	0.935	0.001000	137.8	25.2	2383.8	25.2	2487.4	2512.6	0.091	9.001	6
8	1.072	0.001000	121.0	33.6	2386.6	33.6	2482.6	2516.2	0.121	8.951	8
10	1.227	0.001000	106.4	42.0	2389.3	42.0	2477.9	2519.9	0.151	8.902	10
12	1.401	0.001000	93.8	50.4	2392.1	50.4	2473.2	2523.6	0.180	8.854	12
14	1.597	0.001001	82.9	58.8	2394.8	58.8	2468.5	2527.2	0.210	8.806	14
16	1.817	0.001001	73.4	67.1	2397.6	67.1	2463.8	2530.9	0.239	8.759	16
18	2.062	0.001001	65.1	75.5	2400.3	75.5	2459.0	2534.5	0.268	8.713	18
20	2.34	0.001002	57.8	83.9	2403.0	83.9	2454.3	2538.2	0.296	8.668	20
22	2.64	0.001002	51.5	92.2	2405.8	92.2	2449.6	2541.8	0.325	8.624	22
24	2.98	0.001003	45.9	100.6	2408.5	100.6	2444.9	2545.5	0.353	8.581	24
25	3.17	0.001003	43.4	104.8	2409.9	104.8	2442.5	2547.3	0.367	8.559	25
26	3.36	0.001003	41.0	108.9	2411.2	108.9	2440.2	2549.1	0.381	8.538	26
28	3.78	0.001004	36.7	117.3	2414.0	117.3	2435.4	2552.7	0.409	8.496	28
30	4.24	0.001004	32.9	125.7	2416.7	125.7	2430.7	2556.4	0.437	8.455	30
32	4.75	0.001005	29.6	134.0	2419.4	134.0	2425.9	2560.0	0.464	8.414	32
34	5.32	0.001006	26.6	142.4	2422.1	142.4	2421.2	2563.6	0.491	8.374	34
36	5.94	0.001006	24.0	150.7	2424.8	150.7	2416.4	2567.2	0.518	8.335	36
38	6.62	0.001007	21.6	159.1	2427.5	159.1	2411.7	2570.8	0.545	8.296	38
40	7.38	0.001008	19.55	167.4	2430.2	167.4	2406.9	2574.4	0.572	8.258	40
42	8.20	0.001009	17.69	175.8	2432.9	175.8	2402.1	2577.9	0.599	8.221	42
44	9.10	0.001009	16.04	184.2	2435.6	184.2	2397.3	2581.5	0.625	8.184	44
46	10.09	0.001010	14.56	192.5	2438.3	192.5	2392.5	2585.1	0.651	8.148	46
48	11.16	0.001011	13.23	200.9	2440.9	200.9	2387.7	2588.6	0.678	8.113	48

t	p	v_f	v_g	u_f	u_g	h_f	h_{fd}	h_g	s_f	s_g	t
50	12.34	0.001012	12.05	209.2	2443.6	200.3	2382.9	2592.2	0.704	8.078	50
52	13.61	0.001013	10.98	217.6	2446.2	217.6	2378.1	2595.7	0.729	8.043	52
54	15.00	0.001014	10.02	226.0	2448.9	226.0	2373.2	2599.2	0.755	8.009	54
56	16.51	0.001015	9.16	234.3	2451.5	234.4	2368.4	2602.7	0.780	7.976	56
58	18.15	0.001016	8.38	242.7	2454.1	242.7	2363.5	2606.2	0.806	7.943	58
60	19.92	0.001017	7.68	251.1	2456.8	251.1	2358.6	2609.7	0.831	7.911	60
62	21.84	0.001018	7.04	259.4	2459.4	259.5	2353.7	2613.2	0.856	7.879	62
64	23.91	0.001019	6.47	267.8	2462.0	267.8	2348.8	2616.6	0.881	7.848	64
66	26.15	0.001020	5.95	276.2	2464.5	276.2	2343.9	2620.1	0.906	7.817	66
68	28.56	0.001022	5.48	284.6	2467.1	284.6	2338.9	2623.5	0.930	7.786	68
70	31.16	0.001023	5.05	292.9	2469.7	293.0	2334.0	2626.9	0.955	7.756	70
72	33.96	0.001024	4.66	301.3	2472.2	301.4	2329.0	2630.3	0.979	7.727	72
74	36.96	0.001025	4.30	309.7	2474.8	309.7	2324.0	2633.7	1.003	7.698	74
76	40.19	0.001027	3.98	318.1	2477.3	318.1	2318.9	2637.1	1.027	7.669	76
78	43.65	0.001028	3.68	326.5	2479.8	326.5	2313.9	2640.4	1.051	7.641	78
80	47.36	0.001029	3.41	334.9	2482.3	334.9	2308.8	2643.8	1.075	7.613	80
82	51.33	0.001031	3.16	343.3	2484.8	343.3	2303.8	2647.1	1.099	7.586	82
84	55.57	0.001032	2.93	351.7	2487.3	351.7	2298.6	2650.4	1.123	7.559	84
86	60.11	0.001033	2.73	360.1	2489.7	360.1	2293.5	2653.6	1.146	7.532	86
88	64.95	0.001035	2.54	368.5	2492.2	368.5	2288.4	2656.9	1.169	7.506	88
90	70.11	0.001036	2.36	376.9	2494.6	376.9	2283.2	2660.1	1.193	7.480	90
92	75.61	0.001038	2.20	385.3	2497.0	385.4	2278.0	2663.4	1.216	7.454	92
94	81.46	0.001039	2.05	393.7	2499.4	393.8	2272.8	2666.6	1.239	7.429	94
96	87.69	0.001041	1.915	402.1	2501.8	402.2	2267.5	2669.7	1.261	7.404	96
98	94.30	0.001042	1.789	410.5	2504.1	410.6	2262.2	2672.9	1.284	7.380	98
100	101.325	0.001044	1.673	419.0	2506.5	419.1	2256.9	2676.0	1.307	7.355	100

TABLE 8. SATURATED WATER AND STEAM

PRESSURES FROM THE TRIPLE POINT UP TO 100 kN/m² (1 BAR)[100 kN/m² = 1 bar ≈ 14.5 lbf/in²]

Pressure kN/m ² <i>p</i>	Celsius temp., °C <i>t</i>	Specific volume m ³ /kg		Specific internal energy kJ/kg		Specific enthalpy kJ/kg		Specific entropy kJ/kg K		Pressure kN/m ² <i>p</i>
		Water <i>v_f</i>	Steam <i>v_g</i>	Water <i>u_f</i>	Steam <i>u_g</i>	Water <i>h_f</i>	Evaporation <i>h_{fg}</i>	Water <i>s_f</i>	Steam <i>s_g</i>	
0.611	0.01	0.001000	206.2	zero	2375.6	+0.0	2501.6	zero	9.157	0.611 Triple point
0.8	3.8	0.001000	159.7	15.8	2380.7	15.8	2492.6	0.058	9.058	0.8
1.0	7.0	0.001000	129.2	29.3	2385.2	29.3	2485.0	0.106	8.977	1.0 0.01 bar
1.2	9.7	0.001000	108.7	40.6	2388.9	40.6	2478.7	0.146	8.910	1.2
1.4	12.0	0.001000	93.9	50.3	2392.0	50.3	2473.2	0.180	8.854	1.4
1.6	14.0	0.001001	82.8	58.9	2394.8	58.9	2468.4	0.210	8.805	1.6
1.8	15.9	0.001001	74.0	66.5	2397.4	66.5	2464.1	0.237	8.763	1.8
2.0	17.5	0.001001	67.0	73.5	2399.6	73.5	2460.2	0.261	8.725	2.0
2.2	19.0	0.001002	61.2	79.8	2401.7	79.8	2456.6	0.282	8.690	2.2
2.4	20.4	0.001002	56.4	85.7	2403.6	85.7	2453.3	0.302	8.659	2.4
2.6	21.7	0.001002	52.3	91.1	2405.4	91.1	2450.2	0.321	8.630	2.6
2.8	23.0	0.001002	48.7	96.2	2407.1	96.2	2447.3	0.338	8.603	2.8
3.0	24.1	0.001003	45.7	101.0	2408.6	101.0	2444.6	0.354	8.578	3.0
3.5	26.7	0.001003	39.5	111.8	2412.2	111.8	2438.5	0.391	8.523	3.5
4.0	29.0	0.001004	34.8	121.4	2415.3	121.4	2433.1	0.422	8.475	4.0
4.5	31.0	0.001005	31.1	130.0	2418.1	130.0	2428.2	0.451	8.433	4.5
5.0	32.9	0.001005	28.2	137.8	2420.6	137.8	2423.8	0.476	8.396	5.0
6	36.2	0.001006	23.74	151.5	2425.1	151.5	2416.0	0.521	8.331	6
7	39.0	0.001007	20.53	163.4	2428.9	163.4	2409.2	0.559	8.277	7
8	41.5	0.001008	18.10	173.9	2432.3	173.9	2403.2	0.593	8.230	8
9	43.8	0.001009	16.20	183.3	2435.3	183.3	2397.9	0.622	8.188	9
10	45.8	0.001010	14.67	191.8	2438.0	191.8	2392.9	0.649	8.151	10 0.1 bar
11	47.7	0.001011	13.42	199.7	2440.5	199.7	2388.4	0.674	8.118	11
12	49.4	0.001012	12.36	206.9	2442.8	206.9	2384.3	0.696	8.087	12
13	51.1	0.001013	11.47	213.7	2445.0	213.7	2380.4	0.717	8.059	13
14	52.6	0.001013	10.69	220.0	2447.0	220.0	2376.7	0.737	8.033	14
15	54.0	0.001014	10.02	226.0	2448.9	226.0	2373.2	0.755	8.009	15

Pressure in kN/m²

p	z	v_f	v_g	u_f	u_g	h_f	h_{fg}	h_g	s_f	s_g	p
16	55.3	0.001015	9.43	231.6	2450.6	231.6	2370.0	2601.6	0.772	7.987	16
17	56.6	0.001015	8.91	236.9	2452.3	236.9	2366.9	2603.8	0.788	7.966	17
18	57.8	0.001016	8.45	242.0	2453.9	242.0	2363.9	2605.9	0.804	7.946	18
19	59.0	0.001017	8.03	246.8	2455.4	246.8	2361.1	2607.9	0.818	7.927	19
20	60.1	0.001017	7.65	251.4	2456.9	251.5	2358.4	2609.9	0.832	7.909	20
22	62.2	0.001018	7.00	260.1	2459.6	260.1	2353.3	2613.5	0.858	7.876	22
24	64.1	0.001019	6.45	268.2	2462.1	268.2	2348.6	2616.8	0.882	7.846	24
26	65.9	0.001020	5.98	275.6	2464.4	275.7	2344.2	2619.9	0.904	7.819	26
28	67.5	0.001021	5.58	282.7	2466.5	282.7	2340.0	2622.7	0.925	7.793	28
30	69.1	0.001022	5.23	289.3	2468.6	289.3	2336.1	2625.4	0.944	7.770	30
35	72.7	0.001025	4.53	304.3	2473.1	304.3	2327.2	2631.5	0.988	7.717	35
40	75.9	0.001027	3.99	317.6	2477.1	317.7	2319.2	2636.9	1.026	7.671	40
45	78.7	0.001028	3.58	329.6	2480.7	329.6	2312.0	2641.7	1.060	7.631	45
50	81.3	0.001030	3.24	340.5	2484.0	340.6	2305.4	2646.0	1.091	7.595	50
55	83.7	0.001032	2.96	350.6	2486.9	350.6	2299.3	2649.9	1.119	7.562	55
60	86.0	0.001033	2.73	359.9	2489.7	359.9	2293.6	2653.6	1.145	7.533	60
65	88.0	0.001035	2.53	368.5	2492.2	368.6	2288.3	2656.9	1.170	7.506	65
70	90.0	0.001036	2.36	376.7	2494.5	376.8	2283.3	2660.1	1.192	7.480	70
75	91.8	0.001037	2.22	384.4	2496.7	384.5	2278.6	2663.0	1.213	7.457	75
80	93.5	0.001039	2.087	391.6	2498.8	391.7	2274.1	2665.8	1.233	7.435	80
85	95.2	0.001040	1.972	398.5	2500.8	398.6	2269.8	2668.4	1.252	7.415	85
90	96.7	0.001041	1.869	405.1	2502.6	405.2	2265.6	2670.9	1.270	7.395	90
95	98.2	0.001042	1.777	411.4	2504.4	411.5	2261.7	2673.2	1.287	7.377	95
100	99.6	0.001043	1.694	417.4	2506.1	417.5	2257.9	2675.4	1.303	7.360	100
101.325	100.0	0.001044	1.673	419.0	2506.5	419.1	2256.9	2676.0	1.307	7.355	101.325

Pressure in kN/m²

TABLE 8 (cont.). SATURATED WATER AND STEAM
PRESSURES FROM 0.1 TO 3.0 MN/m² (1 TO 30 BAR)

[0.1 MN/m ² = 1 bar ≈ 14.5 lbf/in ²]											
Pressure MN/m ² <i>p</i>	Celsius temp., °C <i>t</i>	Specific volume m ³ /kg		Specific internal energy kJ/kg		Specific enthalpy kJ/kg			Specific entropy kJ/kg K		Pressure MN/m ² <i>p</i>
		Water <i>v_f</i>	Steam <i>v_g</i>	Water <i>u_f</i>	Steam <i>u_g</i>	Water <i>h_f</i>	Evaporation <i>h_{fg}</i>	Steam <i>h_g</i>	Water <i>s_f</i>	Steam <i>s_g</i>	
0.10	99.6	0.001043	1.694	417.4	2506.1	417.5	2257.9	2675.4	1.303	7.360	0.10
0.11	102.3	0.001046	1.549	428.7	2509.2	428.8	2250.8	2679.6	1.333	7.328	0.11
0.12	104.8	0.001048	1.428	439.2	2512.1	439.4	2244.1	2683.4	1.361	7.298	0.12
0.13	107.1	0.001049	1.325	449.1	2514.7	449.2	2237.8	2687.0	1.387	7.271	0.13
0.14	109.3	0.001051	1.236	458.3	2517.2	458.4	2231.9	2690.3	1.411	7.247	0.14
0.15	111.4	0.001053	1.159	467.0	2519.5	467.1	2226.2	2693.4	1.434	7.223	0.15
0.16	113.3	0.001055	1.091	475.2	2521.7	475.4	2220.9	2696.2	1.455	7.202	0.16
0.17	115.2	0.001056	1.031	483.0	2523.7	483.2	2215.7	2699.0	1.475	7.181	0.17
0.18	116.9	0.001058	0.977	490.5	2525.6	490.7	2210.8	2701.5	1.494	7.162	0.18
0.19	118.6	0.001059	0.929	497.6	2527.5	497.8	2206.1	2704.0	1.513	7.144	0.19
0.20	120.2	0.001061	0.885	504.5	2529.2	504.7	2201.6	2706.3	1.530	7.127	0.20
0.22	123.3	0.001064	0.810	517.4	2532.4	517.6	2193.0	2710.6	1.563	7.095	0.22
0.24	126.1	0.001066	0.746	529.4	2535.4	529.6	2184.9	2714.5	1.593	7.066	0.24
0.26	128.7	0.001069	0.693	540.6	2538.1	540.9	2177.3	2718.2	1.621	7.039	0.26
0.28	131.2	0.001071	0.646	551.1	2540.6	551.4	2170.1	2721.5	1.647	7.014	0.28
0.30	133.5	0.001074	0.606	561.1	2543.0	561.4	2163.2	2724.7	1.672	6.991	0.30
0.32	135.8	0.001076	0.570	570.6	2545.2	570.9	2156.7	2727.6	1.695	6.969	0.32
0.34	137.9	0.001078	0.538	579.6	2547.2	579.9	2150.4	2730.3	1.717	6.949	0.34
0.36	139.9	0.001080	0.510	588.1	2549.2	588.5	2144.4	2732.9	1.738	6.930	0.36
0.38	141.8	0.001082	0.485	596.4	2551.0	596.8	2138.6	2735.3	1.757	6.912	0.38
0.40	143.6	0.001084	0.462	604.2	2552.7	604.7	2133.0	2737.6	1.776	6.894	0.40
0.42	145.4	0.001086	0.442	611.8	2554.4	612.3	2127.5	2739.8	1.795	6.878	0.42
0.44	147.1	0.001088	0.423	619.1	2555.9	619.6	2122.3	2741.9	1.812	6.862	0.44
0.46	148.7	0.001089	0.405	626.2	2557.4	626.7	2117.2	2743.9	1.829	6.847	0.46
0.48	150.3	0.001091	0.389	633.0	2558.8	633.5	2112.2	2745.7	1.845	6.833	0.48
0.50	151.8	0.001093	0.375	639.6	2560.2	640.1	2107.4	2747.5	1.860	6.819	0.50
0.55	155.5	0.001097	0.342	655.2	2563.3	655.8	2095.9	2751.7	1.897	6.787	0.55
0.60	158.8	0.001101	0.315	669.8	2566.2	670.4	2085.0	2755.5	1.931	6.758	0.60
0.65	162.0	0.001105	0.292	683.4	2568.7	684.1	2074.7	2758.9	1.962	6.730	0.65
0.70	165.0	0.001108	0.273	696.3	2571.1	697.1	2064.9	2762.0	1.992	6.705	0.70

Pressure in MN/m²

p	t	v_f	v_g	u_f	u_g	h_f	h_{fg}	h_g	s_f	s_g	p
0.75	167.8	0.001112	0.2554	708.5	2573.3	709.3	2055.5	2764.8	2.020	6.682	0.75
0.80	170.4	0.001115	0.2403	720.0	2575.3	720.9	2046.5	2767.5	2.046	6.660	0.80
0.85	172.9	0.001118	0.2268	731.1	2577.1	732.0	2037.9	2769.9	2.071	6.639	0.85
0.90	175.4	0.001121	0.2148	741.6	2578.8	742.6	2029.5	2772.1	2.094	6.619	0.90
0.95	177.7	0.001124	0.2040	751.8	2580.4	752.8	2021.4	2774.2	2.117	6.601	0.95
1.00	179.9	0.001127	0.1943	761.5	2581.9	762.6	2013.6	2776.2	2.138	6.583	1.00
10 bar											
1.05	182.0	0.001130	0.1855	770.8	2583.3	772.0	2005.9	2778.0	2.159	6.566	1.05
1.10	184.1	0.001133	0.1774	779.9	2584.5	781.1	1998.5	2779.7	2.179	6.550	1.10
1.15	186.0	0.001136	0.1700	788.6	2585.8	789.9	1991.3	2781.3	2.198	6.534	1.15
1.20	188.0	0.001139	0.1632	797.1	2586.9	798.4	1984.3	2782.7	2.216	6.519	1.20
1.25	189.8	0.001141	0.1569	805.3	2588.0	806.7	1977.4	2784.1	2.234	6.505	1.25
1.30	191.6	0.001144	0.1511	813.2	2589.0	814.7	1970.7	2785.4	2.251	6.491	1.30
20 bar											
1.4	195.0	0.001149	0.1407	828.5	2590.8	830.1	1957.7	2787.8	2.284	6.465	1.4
1.5	198.3	0.001154	0.1317	842.9	2592.4	844.7	1945.2	2789.9	2.314	6.441	1.5
1.6	201.4	0.001159	0.1237	856.7	2593.8	858.6	1933.2	2791.7	2.344	6.418	1.6
1.7	204.3	0.001163	0.1166	869.9	2595.1	871.8	1921.5	2793.4	2.371	6.396	1.7
1.8	207.1	0.001168	0.1103	882.5	2596.3	884.6	1910.3	2794.8	2.398	6.375	1.8
1.9	209.8	0.001172	0.1047	894.6	2597.3	896.8	1899.3	2796.1	2.423	6.355	1.9
30 bar											
2.0	212.4	0.001177	0.0995	906.2	2598.2	908.6	1888.6	2797.2	2.447	6.337	2.0
2.1	214.9	0.001181	0.0949	917.5	2598.9	920.0	1878.2	2798.2	2.470	6.319	2.1
2.2	217.2	0.001185	0.0907	928.3	2599.6	931.0	1868.1	2799.1	2.492	6.301	2.2
2.3	219.6	0.001189	0.0868	938.9	2600.2	941.6	1858.2	2799.8	2.514	6.285	2.3
2.4	221.8	0.001193	0.0832	949.1	2600.7	951.9	1848.5	2800.4	2.534	6.269	2.4
40 bar											
2.5	223.9	0.001197	0.0799	959.0	2601.2	962.0	1839.0	2800.9	2.554	6.254	2.5
2.6	226.0	0.001201	0.0769	968.6	2601.5	971.7	1829.6	2801.4	2.574	6.239	2.6
2.7	228.1	0.001205	0.0740	978.0	2601.8	981.2	1820.5	2801.7	2.592	6.224	2.7
2.8	230.0	0.001209	0.0714	987.1	2602.1	990.5	1811.5	2802.0	2.611	6.210	2.8
2.9	232.0	0.001213	0.0689	996.0	2602.3	999.5	1802.6	2802.2	2.628	6.197	2.9
3.0	233.8	0.001216	0.0666	1004.7	2602.4	1008.4	1793.9	2802.3	2.646	6.184	3.0

Pressure in MN/m²

TABLE 8 (cont.). SATURATED WATER AND STEAM
PRESSURES FROM 3 MN/m² TO THE CRITICAL POINT (30 TO 221.2 BAR)

[0.1 MN/m² = 1 bar $\approx$ 14.5 lbf/in²]

Pressure MN/m ² p	Celsius temp., °C t	Specific volume m ³ /kg		Specific internal energy kJ/kg		Specific enthalpy kJ/kg			Specific entropy kJ/kg K		Pressure MN/m ² p
		Water v_f	Steam v_g	Water u_f	Steam u_g	Water h_f	Evaporation h_{fg}	Steam h_g	Water s_f	Steam s_g	
3.0	233.8	0.001216	0.0666	1004.7	2602.4	1008.4	1793.9	2802.3	2.646	6.184	3.0
3.2	237.4	0.001224	0.0624	1021.5	2602.5	1025.4	1776.9	2802.3	2.679	6.158	3.2
3.4	240.9	0.001231	0.0587	1037.6	2602.5	1041.8	1760.3	2802.1	2.710	6.134	3.4
3.6	244.2	0.001238	0.0554	1053.1	2602.2	1057.6	1744.2	2801.7	2.740	6.112	3.6
3.8	247.3	0.001245	0.0524	1068.0	2601.9	1072.7	1728.4	2801.1	2.769	6.090	3.8
4.0	250.3	0.001252	0.0497	1082.4	2601.3	1087.4	1712.9	2800.3	2.797	6.069	4.0
4.2	253.2	0.001259	0.0473	1096.3	2600.7	1101.6	1697.8	2799.4	2.823	6.048	4.2
4.4	256.0	0.001266	0.0451	1109.8	2599.9	1115.4	1682.9	2798.3	2.849	6.029	4.4
4.6	258.8	0.001272	0.0430	1122.9	2599.1	1128.8	1668.3	2797.1	2.873	6.010	4.6
4.8	261.4	0.001279	0.0412	1135.6	2598.1	1141.8	1653.9	2795.7	2.897	5.991	4.8
5.0	263.9	0.001286	0.0394	1148.0	2597.0	1154.5	1639.7	2794.2	2.921	5.974	5.0
5.2	266.4	0.001292	0.0378	1160.1	2595.9	1166.8	1625.7	2792.6	2.943	5.956	5.2
5.4	268.8	0.001299	0.0363	1171.9	2594.6	1178.9	1611.9	2790.8	2.965	5.939	5.4
5.6	271.1	0.001306	0.0349	1183.5	2593.3	1190.8	1598.2	2789.0	2.986	5.923	5.6
5.8	273.3	0.001312	0.0337	1194.7	2591.9	1202.3	1584.7	2787.0	3.007	5.907	5.8
6.0	275.6	0.001319	0.0324	1205.8	2590.4	1213.7	1571.3	2785.0	3.027	5.891	6.0
6.2	277.7	0.001325	0.0313	1216.6	2588.8	1224.8	1558.0	2782.9	3.047	5.875	6.2
6.4	279.8	0.001332	0.0302	1227.2	2587.2	1235.7	1544.9	2780.6	3.066	5.860	6.4
6.6	281.8	0.001338	0.0292	1237.6	2585.5	1246.5	1531.9	2778.3	3.085	5.845	6.6
6.8	283.8	0.001345	0.0283	1247.9	2583.7	1257.0	1518.9	2775.9	3.104	5.831	6.8
7.0	285.8	0.001351	0.0274	1258.0	2581.8	1267.4	1506.0	2773.5	3.122	5.816	7.0
7.2	287.7	0.001358	0.0265	1267.9	2579.9	1277.6	1493.3	2770.9	3.140	5.802	7.2
7.4	289.6	0.001364	0.0257	1277.6	2578.0	1287.7	1480.5	2768.3	3.157	5.788	7.4
7.6	291.4	0.001371	0.0249	1287.2	2575.9	1297.6	1467.9	2765.5	3.174	5.774	7.6
7.8	293.2	0.001378	0.0242	1296.7	2573.8	1307.4	1455.3	2762.8	3.191	5.761	7.8
8.0	295.0	0.001384	0.0235	1306.0	2571.7	1317.1	1442.8	2759.9	3.208	5.747	8.0
8.2	296.7	0.001391	0.0229	1315.2	2569.5	1326.6	1430.3	2757.0	3.224	5.734	8.2
8.4	298.4	0.001398	0.0222	1324.3	2567.2	1336.1	1417.9	2754.0	3.240	5.721	8.4
8.6	300.1	0.001404	0.0216	1333.3	2564.9	1345.4	1405.5	2750.9	3.256	5.708	8.6
8.8	301.7	0.001411	0.0210	1342.2	2562.6	1354.6	1393.2	2747.8	3.271	5.695	8.8

Pressure in MN/m²

p	t	v_f	v_g	u_f	u_g	h_f	h_{fg}	h_g	s_f	s_g	p
9.0	303.3	0.001418	0.02050	1351.0	2560.1	1363.7	1380.9	2744.6	3.287	5.682	9.0
9.2	304.9	0.001425	0.01996	1359.7	2557.7	1372.8	1368.6	2741.4	3.302	5.669	9.2
9.4	306.4	0.001432	0.01945	1368.2	2555.2	1381.7	1356.3	2738.0	3.317	5.657	9.4
9.6	308.0	0.001439	0.01897	1376.7	2552.6	1390.6	1344.1	2734.7	3.332	5.644	9.6
9.8	309.5	0.001446	0.01849	1385.2	2550.0	1399.3	1331.9	2731.2	3.346	5.632	9.8
10.0	311.0	0.001453	0.01804	1393.5	2547.3	1408.0	1319.7	2727.7	3.361	5.620	10.0
10.5	314.6	0.001470	0.01698	1414.1	2540.4	1429.5	1289.2	2718.7	3.396	5.589	10.5
11.0	318.0	0.001489	0.01601	1434.2	2533.2	1450.6	1258.7	2709.3	3.430	5.560	11.0
11.5	321.4	0.001507	0.01511	1454.0	2525.7	1471.3	1228.2	2699.5	3.464	5.530	11.5
12.0	324.6	0.001527	0.01428	1473.4	2517.8	1491.8	1197.4	2689.2	3.497	5.500	12.0
12.5	327.8	0.001547	0.01351	1492.7	2509.4	1512.0	1166.4	2678.4	3.530	5.471	12.5
13.0	330.8	0.001567	0.01280	1511.6	2500.6	1532.0	1135.0	2667.0	3.562	5.441	13.0
13.5	333.8	0.001588	0.01213	1530.4	2491.3	1551.9	1103.1	2655.0	3.593	5.411	13.5
14.0	336.6	0.001611	0.01150	1549.1	2481.4	1571.6	1070.7	2642.4	3.624	5.380	14.0
14.5	339.4	0.001634	0.01090	1567.6	2471.0	1591.3	1037.7	2629.1	3.655	5.349	14.5
15.0	342.1	0.001658	0.01034	1586.1	2459.9	1611.0	1004.0	2615.0	3.686	5.318	15.0
15.5	344.8	0.001683	0.00981	1604.6	2448.2	1630.7	969.6	2600.3	3.716	5.286	15.5
16.0	347.3	0.001710	0.00931	1623.2	2436.0	1650.5	934.3	2584.9	3.747	5.253	16.0
16.5	349.8	0.001739	0.00883	1641.8	2423.1	1670.5	898.3	2568.8	3.778	5.220	16.5
17.0	352.3	0.001770	0.00837	1661.6	2409.3	1691.7	859.9	2551.6	3.811	5.185	17.0
17.5	354.6	0.001803	0.00793	1681.8	2394.6	1713.3	820.0	2533.3	3.844	5.150	17.5
18.0	357.0	0.001840	0.00750	1701.7	2378.9	1734.8	779.1	2513.9	3.877	5.113	18.0
18.5	359.2	0.001881	0.00708	1721.7	2362.1	1756.5	736.6	2493.1	3.909	5.074	18.5
19.0	361.4	0.001926	0.00668	1742.1	2343.8	1778.7	692.0	2470.6	3.943	5.033	19.0
19.5	363.6	0.001977	0.00628	1763.2	2323.6	1801.8	644.2	2446.0	3.978	4.989	19.5
20.0	365.7	0.00204	0.00588	1785.7	2300.8	1826.5	591.9	2418.4	4.015	4.941	20.0
20.5	367.8	0.00211	0.00546	1810.7	2274.4	1853.9	532.5	2386.4	4.056	4.887	20.5
21.0	369.8	0.00220	0.00502	1840.0	2242.1	1886.3	461.3	2347.6	4.105	4.822	21.0
21.5	371.8	0.00234	0.00451	1878.6	2198.1	1928.9	366.2	2295.2	4.169	4.737	21.5
22.0	373.7	0.00267	0.00373	1952	2114	2011	185	2196	4.295	4.580	22.0
22.12	374.15	0.00317	0.00317	2038	2038	2108	0	2108	4.444	4.444	22.12
Critical point											

Pressure in MN/m²

TABLE 10. SPECIFIC ENTROPY OF WATER AND STEAM

		[0.1 MN/m ² = 1 bar ≈ 14.5 lbf/in ²]																Celsius temp., °C		
		isobar																		
Pressure/(MN/m ²) Pressure/bar	Sat. Celsius temp., °C { Water Steam	0	0.01	0.05	0.1	0.5	1	2	4	6	8	10	15	20	22.12	25	30	40	50	100
		0	0.1	1	10	100	1000	10000	100000	1000000	10000000	100000000	1000000000	10000000000	100000000000	1000000000000	10000000000000	100000000000000	1000000000000000	10000000000000000
0	45.8	81.3	99.6	151.8	179.9	212.4	250.3	275.6	295.6	311.0	342.1	365.7	374.15	—	—	—	—	—	—	—
0	0.649	1.091	1.303	1.860	2.138	2.447	2.797	3.027	3.208	3.361	3.686	4.015	4.444	—	—	—	—	—	—	—
0	8.151	7.595	7.360	6.819	6.583	6.337	6.069	5.891	5.747	5.600	5.318	4.941	4.444	—	—	—	—	—	—	—
Specific entropy/(kJ/kg K)																				
0	0	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.001	0.001	0.001	0.001	0.001	0.001	0.001	0.000	0.000	0.007
25	0.367	0.367	0.367	0.367	0.367	0.366	0.366	0.365	0.365	0.364	0.363	0.362	0.361	0.360	0.359	0.356	0.353	0.336	0.336	0.336
50	0.703	0.703	0.703	0.703	0.703	0.702	0.702	0.701	0.700	0.699	0.697	0.694	0.693	0.692	0.690	0.685	0.681	0.658	0.658	0.658
75	1.015	1.015	1.015	1.015	1.015	1.014	1.013	1.012	1.010	1.009	1.006	1.003	1.002	1.000	0.997	0.991	0.985	0.958	0.958	0.958
100	1.307	1.306	1.305	1.304	1.302	1.301	1.299	1.295	1.292	1.290	1.288	1.284	1.277	1.270	1.263	1.246	1.237	1.237	1.237	1.237
125	1.581	1.581	1.580	1.578	1.576	1.574	1.572	1.568	1.563	1.561	1.559	1.555	1.546	1.538	1.530	1.521	1.508	1.508	1.508	1.508
150	1.842	1.841	1.840	1.838	1.836	1.833	1.831	1.826	1.821	1.819	1.816	1.811	1.801	1.791	1.778	1.768	1.753	1.753	1.753	1.753
175	2.091	2.089	2.087	2.084	2.081	2.079	2.077	2.073	2.066	2.064	2.061	2.055	2.043	2.032	2.019	2.006	1.991	1.991	1.991	1.991
200	2.330	2.327	2.324	2.321	2.318	2.316	2.313	2.308	2.303	2.300	2.296	2.289	2.276	2.263	2.249	2.235	2.219	2.219	2.219	2.219
225	2.561	2.557	2.554	2.551	2.548	2.545	2.541	2.536	2.531	2.527	2.522	2.515	2.501	2.486	2.471	2.454	2.436	2.436	2.436	2.436
250	2.793	2.789	2.784	2.779	2.774	2.769	2.764	2.758	2.753	2.747	2.741	2.734	2.719	2.703	2.687	2.669	2.650	2.650	2.650	2.650
275	3.022	3.018	3.014	3.010	3.006	3.002	3.000	2.995	2.988	2.981	2.974	2.966	2.956	2.943	2.930	2.916	2.899	2.899	2.899	2.899
300	3.249	3.245	3.241	3.237	3.232	3.228	3.223	3.217	3.210	3.203	3.196	3.187	3.176	3.163	3.149	3.134	3.116	3.116	3.116	3.116
325	3.476	3.471	3.467	3.462	3.457	3.452	3.446	3.439	3.432	3.425	3.417	3.406	3.394	3.380	3.365	3.349	3.330	3.330	3.330	3.330
350	3.703	3.697	3.693	3.688	3.683	3.677	3.670	3.662	3.654	3.646	3.637	3.625	3.612	3.597	3.581	3.564	3.545	3.545	3.545	3.545
375	3.930	3.924	3.919	3.914	3.908	3.902	3.895	3.886	3.877	3.868	3.858	3.846	3.832	3.816	3.799	3.781	3.761	3.761	3.761	3.761
400	4.157	4.151	4.146	4.140	4.134	4.127	4.120	4.111	4.102	4.092	4.081	4.069	4.054	4.037	4.019	3.999	3.974	3.974	3.974	3.974
425	4.384	4.378	4.372	4.366	4.359	4.352	4.344	4.335	4.325	4.314	4.302	4.289	4.273	4.255	4.236	4.215	4.189	4.189	4.189	4.189
450	4.611	4.604	4.598	4.591	4.583	4.575	4.566	4.556	4.545	4.533	4.520	4.506	4.490	4.471	4.451	4.429	4.401	4.401	4.401	4.401
475	4.838	4.831	4.824	4.817	4.809	4.800	4.790	4.779	4.767	4.754	4.740	4.725	4.708	4.689	4.668	4.645	4.616	4.616	4.616	4.616
500	5.065	5.058	5.050	5.042	5.033	5.023	5.012	5.000	4.987	4.973	4.958	4.942	4.924	4.905	4.884	4.861	4.826	4.826	4.826	4.826
550	5.518	5.510	5.501	5.492	5.482	5.471	5.459	5.446	5.431	5.416	5.400	5.383	5.364	5.344	5.322	5.298	5.262	5.262	5.262	5.262
600	5.971	5.962	5.952	5.942	5.931	5.919	5.906	5.891	5.875	5.859	5.842	5.824	5.804	5.782	5.758	5.721	5.685	5.685	5.685	5.685
650	6.424	6.414	6.403	6.392	6.380	6.367	6.352	6.336	6.319	6.301	6.283	6.264	6.243	6.220	6.195	6.167	6.130	6.130	6.130	6.130
700	6.877	6.866	6.854	6.842	6.829	6.815	6.800	6.783	6.765	6.746	6.727	6.707	6.685	6.661	6.635	6.606	6.568	6.568	6.568	6.568
750	7.330	7.318	7.306	7.293	7.279	7.264	7.247	7.229	7.210	7.190	7.170	7.149	7.126	7.101	7.072	7.034	7.000	7.000	7.000	7.000
800	7.783	7.770	7.757	7.743	7.728	7.712	7.694	7.675	7.655	7.634	7.613	7.591	7.567	7.540	7.509	7.478	7.442	7.442	7.442	7.442

TABLE 11. DENSITY OF WATER AND STEAM

Pressure/(MN/m ²) Pressure/bar		[0.1 MN/m ² = 1 bar ≈ 14.5 lbf/in ²]																	Celsius temp., °C	
		C.H. isobar																		
		0	0.01	0.05	0.1	0.5	1	2	4	6	8	10	15	20	22.12	25	30	40	50	100
Sat. Celsius temp., °C		0	0.1	100																1000
Sat. density kg/m ³		—	45.8	81.3	99.6	151.8	179.9	212.4	250.3	275.6	295.0	311.0	342.1	365.7	374.15	—	—	—	—	—
{ Water		—	990	971	958	915	887	850	799	758	722	688	603	491	315	—	—	—	—	—
{ Steam		—	0.0681	0.309	0.590	2.67	5.15	10.05	20.10	30.8	42.5	55.4	96.7	170.2	315	—	—	—	—	—
Celsius temp., °C		Density/(kg/m ³)																		
0	25	50	75	100	125	150	175	200	225	250	275	300	325	350	375	400	425	450	475	500
1000	997	988	975	958	939	917	892	865	835	806	773	735	685	600	491	374	250	170	100	—
997	988	975	958	939	917	892	865	835	806	773	735	685	600	491	374	250	170	100	—	—
988	975	958	939	917	892	865	835	806	773	735	685	600	491	374	250	170	100	—	—	—
975	958	939	917	892	865	835	806	773	735	685	600	491	374	250	170	100	—	—	—	—
958	939	917	892	865	835	806	773	735	685	600	491	374	250	170	100	—	—	—	—	—
939	917	892	865	835	806	773	735	685	600	491	374	250	170	100	—	—	—	—	—	—
917	892	865	835	806	773	735	685	600	491	374	250	170	100	—	—	—	—	—	—	—
892	865	835	806	773	735	685	600	491	374	250	170	100	—	—	—	—	—	—	—	—
865	835	806	773	735	685	600	491	374	250	170	100	—	—	—	—	—	—	—	—	—
835	806	773	735	685	600	491	374	250	170	100	—	—	—	—	—	—	—	—	—	—
806	773	735	685	600	491	374	250	170	100	—	—	—	—	—	—	—	—	—	—	—
773	735	685	600	491	374	250	170	100	—	—	—	—	—	—	—	—	—	—	—	—
735	685	600	491	374	250	170	100	—	—	—	—	—	—	—	—	—	—	—	—	—
685	600	491	374	250	170	100	—	—	—	—	—	—	—	—	—	—	—	—	—	—
600	491	374	250	170	100	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
491	374	250	170	100	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
374	250	170	100	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
250	170	100	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
170	100	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—
100	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—	—

Note: Density is tabulated here, instead of specific volume, since interpolation between pressures is thereby facilitated.

REFRIGERANT TABLES

In Tables 13-16, the arbitrary datum state for zero enthalpy and entropy is that of the saturated liquid at a Celsius temperature of -40°C

TABLE 15. PROPERTIES OF AMMONIA, NH₃[0.1 MN/m² = 1 bar ≈ 14.5 lbf/in²]

Saturation Celsius temp., °C <i>t</i>	Pressure MN/m ² <i>p</i>	Saturated									
		Specific volume m ³ /kg		Specific enthalpy kJ/kg		Specific entropy kJ/kg K		Superheated			
		Liquid <i>v_l</i>	Vapour <i>v_g</i>	Liquid <i>h_l</i>	Vapour <i>h_g</i>	Liquid <i>s_l</i>	Vapour <i>s_g</i>	By 50 K		By 100 K	
								<i>h</i>	<i>s</i>	<i>h</i>	<i>s</i>
-40	0.0718	0.00145	1.552	zero	1390	zero	5.963	1499	6.387	1606	6.736
-35	0.0932	0.00146	1.216	22.3	1398	0.095	5.872	1508	6.292	1616	6.639
-30	0.1196	0.00148	0.963	44.7	1406	0.188	5.785	1517	6.203	1626	6.547
-25	0.1516	0.00149	0.772	67.2	1413	0.279	5.703	1526	6.119	1636	6.461
-20	0.190	0.00150	0.624	89.8	1420	0.368	5.624	1535	6.039	1646	6.379
-15	0.236	0.00152	0.509	112.3	1426	0.457	5.549	1543	5.963	1656	6.301
-10	0.291	0.00153	0.418	135.4	1433	0.544	5.477	1552	5.891	1665	6.227
-5	0.355	0.00155	0.347	158.2	1439	0.630	5.407	1560	5.822	1675	6.157
0	0.429	0.00157	0.289	181.2	1444	0.715	5.340	1568	5.756	1684	6.090
5	0.516	0.00158	0.243	204.5	1450	0.799	5.276	1576	5.694	1693	6.027
10	0.615	0.00160	0.206	227.7	1454	0.881	5.214	1583	5.634	1702	5.967
15	0.728	0.00162	0.175	251.4	1459	0.963	5.154	1590	5.576	1711	5.909
20	0.857	0.00164	0.149	275.2	1463	1.044	5.095	1597	5.521	1719	5.853
25	1.001	0.00166	0.128	298.9	1466	1.124	5.039	1604	5.468	1728	5.800
30	1.167	0.00168	0.111	323.1	1469	1.204	4.984	1610	5.417	1736	5.750
35	1.350	0.00170	0.096	347.5	1471	1.282	4.930	1616	5.368	1744	5.702
40	1.554	0.00173	0.083	371.5	1473	1.360	4.877	1622	5.321	1752	5.655
45	1.782	0.00175	0.073	396.8	1474	1.437	4.825	1628	5.275	1760	5.610
50	2.033	0.00178	0.063	421.9	1475	1.515	4.773	1633	5.230	1767	5.567

Freezing point at 1 atm = -77.7 °C

Critical point: Celsius temp. = 132.4 °C
pressure = 11.30 MN/m² (113.0 bar)

TABLE 16. PROPERTIES OF CARBON DIOXIDE, CO₂

[0.1 MN/m² = 1 bar ≈ 14.5 lbf/in²]

Saturation Celsius temp., °C <i>t</i>	Pressure MN/m ² <i>p</i>	Saturated									
		Specific volume m ³ /kg		Specific enthalpy kJ/kg		Specific entropy kJ/kg K		Superheated			
		Liquid <i>v_l</i>	Vapour <i>v_g</i>	Liquid <i>h_l</i>	Vapour <i>h_g</i>	Liquid <i>s_l</i>	Vapour <i>s_g</i>	By 30 K		By 60 K	
								<i>h</i>	<i>s</i>	<i>h</i>	<i>s</i>
-40	1.005	0.00090	0.0182	zero	321.1	zero	1.377	355.4	1.507	383.0	1.611
-35	1.20	0.00091	0.0320	9.7	322.2	0.039	1.352	356.9	1.485	385.6	1.588
-30	1.43	0.00093	0.0270	19.5	323.1	0.079	1.328	358.7	1.464	388.0	1.566
-25	1.68	0.00095	0.0229	29.5	323.7	0.119	1.304	360.4	1.442	390.3	1.545
-20	1.97	0.00097	0.0195	39.7	323.7	0.158	1.280	361.8	1.421	392.5	1.525
-15	2.29	0.00099	0.0166	50.2	323.2	0.198	1.256	363.0	1.401	394.5	1.505
-10	2.65	0.00102	0.0142	60.9	322.3	0.238	1.231	363.9	1.381	396.2	1.486
-5	3.04	0.00105	0.0122	72.0	320.5	0.278	1.205	364.6	1.361	397.8	1.467
0	3.48	0.00108	0.0104	83.7	318.1	0.320	1.178	364.9	1.342	399.3	1.449
5	3.97	0.00117	0.00879	96.0	312.9	0.364	1.143	364.9	1.322	400.4	1.431
10	4.50	0.00116	0.00743	109.1	307.2	0.407	1.107	364.7	1.302	401.4	1.414
15	5.08	0.00121	0.00623	123.3	301.0	0.454	1.071	364.0	1.282	402.2	1.396
20	5.73	0.00129	0.00516	139.1	292.3	0.506	1.028	362.9	1.261	402.7	1.379
25	6.44	0.00140	0.00413	159.7	279.9	0.573	0.976	361.5	1.241	403.0	1.362
30	7.21	0.00169	0.00294	191.2	253.1	0.682	0.886	359.6	1.220	402.9	1.345
31.05	7.38	0.00214	0.00214	223.0	223.0	0.780	0.780	359.1	1.216	402.9	1.341

Triple point: temperature = -56.6 °C, pressure = 0.518 MN/m²
 Sublimation point at 1 atm = -78.5 °C

Critical point

AIR AT LOW TEMPERATURES

In Tables 17-19, the arbitrary datum state for zero enthalpy and entropy is that of the saturated liquid at a pressure of 0.1 MN/m^2 (1 bar)

TABLE 17. SATURATED LIQUID AND VAPOUR (AIR)

Warning: This table lists *absolute* temperatures.[0.1 MN/m² = 1 bar $\approx$ 14.5 lbf/in²]

Pressure MN/m ² <i>p</i>	Temperature K		Specific volume m ³ /kg		Specific enthalpy kJ/kg		Specific entropy kJ/kg K		Pressure MN/m ² <i>p</i>
	Liquid (bubble)	Vapour (dew)	Liquid <i>v_f</i>	Vapour <i>v_g</i>	Liquid <i>h_f</i>	Vapour <i>h_g</i>	Liquid <i>s_f</i>	Vapour <i>s_g</i>	
0.1	78.7	81.7	0.00114	0.224	zero	205.3	zero	2.559	0.1
0.2	85.4	88.1	0.00118	0.119	11.9	210.5	0.143	2.433	0.2
0.3	90.7	92.5	0.00122	0.081	20.0	213.3	0.234	2.354	0.3
0.5	96.2	98.5	0.00127	0.050	31.7	215.9	0.357	2.249	0.5
0.7	100.8	103.0	0.00132	0.036	41.0	217.0	0.448	2.175	0.7
1.0	106.2	108.1	0.00138	0.0251	53.1	217.1	0.561	2.092	1.0
1.5	113.1	114.7	0.00149	0.0163	70.7	215.5	0.715	1.987	1.5
2.0	118.5	119.8	0.00160	0.0116	86.6	211.7	0.847	1.898	2.0
2.5	123.0	124.1	0.00173	0.0087	101.6	206.3	0.964	1.812	2.5
3.0	127.0	127.8	0.00190	0.0066	116.8	199.0	1.077	1.723	3.0
3.5	130.1	131.1	0.00221	0.0048	134.2	187.7	1.212	1.621	3.5
3.766	132.5 max. point of contact		0.00313		164.4		1.430		3.766
3.774 (max.)	132.4 plait point		0.00305		162.7		1.418		3.774 (max.)

Critical point

TABLE 18. SPECIFIC ENTHALPY OF LIQUID AND VAPOUR (AIR)

Warning: This table lists *absolute* temperatures.[0.1 MN/m² = 1 bar $\approx$ 14.5 lbf/in²]

Pressure MN/m ²	Temperature/K ... 90 100 110 120 125 130 135 140 145 150 160 170 180 190 200 250 300		Sat. temp.		K		Specific enthalpy		Pressure	
	Liq.		Vap.				kJ/kg		MN/m ²	
0.1	78.7	81.7					214.0 224.4 234.8 245.2 250.4 255.6 260.7 265.9 271.1 276.2 286.5 296.7 306.9 317.1 327.2 377.7 427.8		0.1	1 bar
0.5	96.2	98.5					217.9 229.4 240.7 246.2 251.7 257.1 262.4 267.8 273.1 283.7 294.2 304.7 315.1 325.4 376.5 427.2		0.5	5 bar
1	106.2	108.1					219.8 233.1 239.4 245.5 251.4 257.2 263.0 268.7 279.9 290.9 301.7 312.4 323.1 375.0 426.2		1	10 bar
2	118.5	119.8					221.4 230.0 237.8 245.2 252.2 258.9 271.7 283.8 295.6 307.0 318.1 372.0 424.2		2	20 bar
3	127.0	127.8					81.0 103.5 206.6 219.7 230.4 239.5 247.8 262.8 276.4 289.2 301.4 313.1 368.9 422.2		3	30 bar
4							75.6 94.0 117.7 166.5 209.1 223.6 234.6 252.7 268.3 282.4 295.6 308.1 365.8 420.2		4	40 bar
5							73.1 89.7 109.2 134.4 165.4 193.5 215.4 241.1 259.6 275.4 289.7 302.9 362.7 418.1		5	50 bar
10							70.1 83.9 98.1 112.8 128.0 143.7 159.5 190.3 217.2 239.8 259.3 276.7 347.6 408.5		10	100 bar
15							70.4 83.1 95.8 108.6 121.5 134.5 147.5 172.8 196.5 218.5 238.8 257.5 335.1 400.5		15	150 bar
20							72.1 84.0 95.8 107.6 119.4 131.1 142.7 165.5 187.3 208.0 227.6 246.0 325.9 394.3		20	200 bar
25							75.5 86.9 98.2 109.5 120.6 131.5 142.3 163.4 183.8 203.3 221.9 239.8 319.7 389.8		25	250 bar
30							80.0 91.2 102.2 113.0 123.6 134.1 144.3 164.1 183.2 201.7 219.5 236.8 315.9 386.8		30	300 bar
35							166.8 184.8 202.4 219.5 236.2 314.1 385.2		35	350 bar
40							170.5 187.7 204.5 220.9 237.1 313.7 384.9		40	400 bar
45							175.0 191.4 207.6 223.5 239.1 314.5 385.4		45	450 bar
50							179.7 195.4 211.0 226.5 241.7 315.7 386.3		50	500 bar
60							218.3 233.2 247.9 319.9 389.3		60	600 bar
70							240.4 254.8 325.2 393.6		70	700 bar
80							248.3 262.3 331.5 399.1		80	800 bar
90							338.4 405.4		90	900 bar
100							345.5 412.1		100	1000 bar

No

TABLE 19. SPECIFIC ENTROPY OF LIQUID AND VAPOUR (AIR)

TABLE 19. SPECIFIC ENTROPY OF LIQUID AND VAPOUR (AIR)

Warning: This table lists *absolute* temperatures.[0.1 MN/m² = 1 bar $\approx$ 14.5 lbf/in²]

Pressure MN/m ²		Temperature/K ...		90	100	110	120	125	130	135	140	145	150	160	170	180	190	200	250	300	Specific entropy kJ/kg K		Pressure MN/m ²	
		Sat. temp.	K																		Liq.	Vap.	0.1	1 bar
0.1	78.7	81.7	2.660	2.770	2.867	2.957	3.000	3.041	3.080	3.117	3.153	3.188	3.254	3.317	3.375	3.430	3.482	3.708	3.892		0.1	1 bar		
0.5	96.2	98.5		2.267	2.378	2.475	2.520	2.563	2.604	2.643	2.680	2.717	2.785	2.849	2.909	2.965	3.018	3.246	3.431		0.5	5 bar		
1	106.2	108.1			2.116	2.232	2.283	2.331	2.376	2.418	2.458	2.497	2.569	2.636	2.698	2.756	2.810	3.042	3.229		1	10 bar		
2	118.5	119.8				1.977	2.043	2.103	2.157	2.206	2.251	2.333	2.407	2.474	2.536	2.593	2.833	3.024		2	20 bar			
3	127.0	127.8				0.790	0.973	1.182	1.382	1.559	1.702	1.819	1.916	2.000	2.071	2.131	2.181	2.457	2.601		3	30 bar		
4						0.739	0.888	1.074	1.243	1.443	1.652	1.854	1.928	2.045	2.140	2.221	2.292	2.356	2.614	2.812		4	40 bar	
5						0.708	0.844	0.996	1.186	1.413	1.609	1.758	1.924	2.036	2.127	2.204	2.271	2.539	2.741		5	50 bar		
10						0.625	0.737	0.849	0.960	1.070	1.180	1.288	1.486	1.649	1.778	1.884	1.972	2.291	2.513		10	100 bar		
15						0.572	0.675	0.775	0.872	0.966	1.057	1.145	1.308	1.452	1.577	1.687	1.782	2.130	2.369		15	150 bar		
20						0.532	0.630	0.723	0.812	0.898	0.981	1.059	1.206	1.339	1.457	1.563	1.657	2.015	2.265		20	200 bar		
25						0.507	0.601	0.689	0.774	0.855	0.932	1.005	1.142	1.265	1.376	1.477	1.569	1.926	2.182		25	250 bar		
30						0.489	0.581	0.667	0.748	0.826	0.899	0.968	1.095	1.212	1.317	1.414	1.502	1.856	2.115		30	300 bar		
35													1.064	1.173	1.274	1.366	1.451	1.800	2.060		35	350 bar		
40													1.040	1.144	1.240	1.329	1.412	1.754	2.013		40	400 bar		
45													1.020	1.119	1.212	1.298	1.378	1.714	1.973		45	450 bar		
50													1.003	1.099	1.188	1.271	1.350	1.680	1.937		50	500 bar		
60														1.145	1.226	1.301	1.376	1.623	1.876		60	600 bar		
70															1.187	1.261	1.335	1.575	1.825		70	700 bar		
80															1.154	1.226	1.298	1.536	1.781		80	800 bar		
90																		1.499	1.744		90	900 bar		
100																		1.467	1.710		100	1000 bar		

TRANSPORT PROPERTIES OF VARIOUS FLUIDS

In addition to giving values of the transport properties λ , μ and Pr , Tables 20–24 also list values of the thermodynamic properties v and c_p , since these are frequently required in heat transfer calculations.

Warning note:

For convenience of tabulation in Tables 20–24, the **dynamic** viscosity μ is given in g/s m instead of kg/s m ($\equiv$ N s/m²). It should be noted, therefore, that in the calculation of viscous stress through the relation $\tau = \mu \partial V / \partial y$, μ must be in kg/s m if τ is to be in N/m², since 1 N = 1 kg m/s².

Similar care must be exercised when calculating the **kinematic** viscosity ν (in m²/s) from the defining expression, $\nu = \mu / \rho = \mu v$.

TABLE 20. SATURATED WATER AND STEAM

Celsius temp., °C	<i>t</i>	Specific volume m ³ /kg		Isobaric specific heat capacity kJ/kg K		Thermal conductivity W/m K		Dynamic viscosity* g/s m		Prandtl number = $\mu c_p / \lambda$		Celsius temp., °C
		v_f	v_g	$c_{p,f}$	$c_{p,g}$	λ_f	λ_g	μ_f	μ_g	Pr_f	Pr_g	
	0.01	0.00100	206.2	4.217	1.854	0.569	0.0173	1.755	0.0088	13.02	0.942	0.01 Triple point
	10	0.00100	106.4	4.193	1.860	0.587	0.0185	1.301	0.0091	9.29	0.915	10
	20	0.00100	57.8	4.182	1.866	0.603	0.0191	1.002	0.0094	6.95	0.918	20
	30	0.00100	32.9	4.179	1.875	0.618	0.0198	0.797	0.0097	5.39	0.923	30
	40	0.00101	19.5	4.179	1.885	0.632	0.0204	0.651	0.0101	4.31	0.930	40
	50	0.00101	12.05	4.181	1.899	0.643	0.0210	0.544	0.0104	3.53	0.939	50
	60	0.00102	7.68	4.185	1.915	0.653	0.0217	0.462	0.0107	2.96	0.947	60
	70	0.00102	5.05	4.190	1.936	0.662	0.0224	0.400	0.0111	2.53	0.956	70
	80	0.00103	3.41	4.197	1.962	0.670	0.0231	0.350	0.0114	2.19	0.966	80
	90	0.00104	2.36	4.205	1.992	0.676	0.0240	0.311	0.0117	1.93	0.976	90
	100	0.00104	1.673	4.216	2.028	0.681	0.0249	0.278	0.0121	1.723	0.986	100
	125	0.00107	0.770	4.254	2.147	0.687	0.0272	0.219	0.0133	1.358	1.047	125
	150	0.00109	0.392	4.310	2.314	0.687	0.0300	0.180	0.0144	1.133	1.110	150
	175	0.00112	0.217	4.389	2.542	0.679	0.0334	0.153	0.0156	0.990	1.185	175
	200	0.00116	0.127	4.497	2.843	0.665	0.0375	0.133	0.0167	0.902	1.270	200
	225	0.00120	0.0783	4.648	3.238	0.644	0.0427	0.1182	0.0179	0.853	1.36	225
	250	0.00125	0.0500	4.867	3.772	0.616	0.0495	0.1065	0.0191	0.841	1.45	250
	275	0.00132	0.0327	5.202	4.561	0.582	0.0587	0.0972	0.0202	0.869	1.56	275
	300	0.00140	0.0216	5.762	5.863	0.541	0.0719	0.0897	0.0214	0.955	1.74	300
	325	0.00153	0.0142	6.861	8.440	0.493	0.0929	0.0790	0.0230	1.100	2.09	325
	350	0.00174	0.00880	10.10	17.15	0.437	0.1343	0.0648	0.0258	1.50	3.29	350
	360	0.00190	0.00694	14.6	25.1	0.400	0.168	0.0582	0.0275	2.11	3.89	360
	374.15	0.00317	0.00317	∞	∞	0.24	0.24	0.045	0.045	∞	∞	374.15 Critical point

* See warning note on page 31.

TABLE 21. STEAM AT ATMOSPHERIC PRESSURE

[1 atm ≈ 0.101 MN/m² ≈ 14.7 lbf/in²]

Celsius temperature, °C <i>t</i>	Specific volume m ³ /kg <i>v</i>	Isobaric specific heat capacity kJ/kg K <i>c_p</i>	Thermal conductivity W/m K λ	Dynamic viscosity* g/s m μ	Prandtl number $= \mu c_p / \lambda$ <i>Pr</i>	Celsius temperature, °C <i>t</i>
100	1.673	2.028	0.0245	0.0121	1.006	100
200	2.144	1.979	0.0331	0.0162	0.968	200
300	2.604	2.010	0.0434	0.0204	0.946	300
400	3.062	2.067	0.0548	0.0246	0.928	400
500	3.519	2.132	0.0673	0.0288	0.912	500
600	3.975	2.201	0.0805	0.0329	0.898	600
700	4.431	2.268	0.0942	0.0368	0.887	700
800	4.887	2.332	0.1080	0.0406	0.876	800

* See warning note on p. 31.

Values for water at atmospheric pressure between 0 °C and 100 °C are given with sufficient accuracy by the saturation values in Table 20.

TABLE 22. AIR AT ATMOSPHERIC PRESSURE

[1 atm ≈ 0.101 MN/m² ≈ 14.7 lbf/in²]

Celsius temperature, °C <i>t</i>	Specific volume m ³ /kg <i>v</i>	Isobaric specific heat capacity kJ/kg K <i>c_p</i>	Thermal conductivity W/m K λ	Dynamic viscosity* g/s m μ	Prandtl number $= \mu c_p / \lambda$ <i>Pr</i>	Celsius temperature, °C <i>t</i>
-100	0.488	1.01	0.016	0.012	0.75	-100
0	0.773	1.01	0.024	0.017	0.72	0
100	1.057	1.02	0.032	0.022	0.70	100
200	1.341	1.03	0.039	0.026	0.69	200
300	1.624	1.05	0.045	0.030	0.69	300
400	1.908	1.07	0.051	0.033	0.70	400
500	2.191	1.10	0.056	0.036	0.70	500
600	2.473	1.12	0.061	0.039	0.71	600
700	2.756	1.14	0.066	0.042	0.72	700
800	3.039	1.16	0.071	0.044	0.73	800

* See warning note on p. 31.

This Table may be used with reasonable accuracy for values of *c_p*, λ , μ and *Pr* of N₂, O₂ and CO

TABLE 23. CARBON DIOXIDE AT ATMOSPHERIC PRESSURE

[1 atm ≈ 0.101 MN/m ² ≈ 14.7 lbf/in ²]						
Celsius temperature, °C <i>t</i>	Specific volume m ³ /kg <i>v</i>	Isobaric specific heat capacity kJ/kg K <i>c_p</i>	Thermal conductivity W/m K λ	Dynamic viscosity* g/s m μ	Prandtl number $= \mu c_p / \lambda$ <i>Pr</i>	Celsius temperature, °C <i>t</i>
-50	0.410	0.79	0.011	0.011	0.79	-50
0	0.506	0.83	0.015	0.014	0.78	0
100	0.694	0.92	0.022	0.018	0.75	100
200	0.881	1.00	0.030	0.022	0.73	200
300	1.068	1.06	0.038	0.026	0.72	300
400	1.255	1.11	0.046	0.029	0.71	400
500	1.442	1.16	0.053	0.032	0.70	500
600	1.628	1.20	0.061	0.035	0.69	600
700	1.814	1.23	0.069	0.038	0.68	700
800	2.000	1.25	0.078	0.041	0.67	800

* See warning note on p. 31.

TABLE 24. HYDROGEN AT ATMOSPHERIC PRESSURE

[1 atm ≈ 0.101 MN/m ² ≈ 14.7 lbf/in ²]						
Celsius temperature, °C <i>t</i>	Specific volume m ³ /kg <i>v</i>	Isobaric specific heat capacity kJ/kg K <i>c_p</i>	Thermal conductivity W/m K λ	Dynamic viscosity* g/s m μ	Prandtl number $= \mu c_p / \lambda$ <i>Pr</i>	Celsius temperature, °C <i>t</i>
-200	2.97	10.6	0.050	0.0033	0.71	-200
-100	7.05	13.1	0.112	0.0062	0.72	-100
0	11.13	14.2	0.172	0.0084	0.69	0
100	15.19	14.5	0.220	0.0103	0.68	100
200	19.26	14.5	0.264	0.0121	0.67	200
300	23.34	14.5	0.307	0.0138	0.66	300
400	27.41	14.6	0.348	0.0154	0.65	400
500	31.48	14.7	0.387	0.0169	0.64	500
600	35.54	14.8	0.427	0.0183	0.63	600
700	39.61	14.9	0.476	0.0199	0.62	700
800	43.68	15.1	0.528	0.0211	0.61	800

* See warning note on p. 31.

APPENDIX A

DEFINITIONS OF BASIC SI UNITS

The units quoted below are the basic units of the *Système International d'Unités*. The abbreviation CGPM refers to the *Conférence Générale des Poids et Mesures*.

Length: The unit of length called the *metre* is the length of the path travelled by light in vacuum during a time interval of $1/299\,792\,458$ of a second (17th CGPM, 1983).

Mass: The unit of mass called the *kilogram* is the mass of the international prototype which is in the custody of the *Bureau International des Poids et Mesures* (BIPM) at Sèvres, near Paris, France (3rd CGPM, 1901).

Time: The unit of time called the *second* is the duration of $9\,192\,631\,770$ periods of the radiation corresponding to the transition between the two hyperfine levels of the ground state of the caesium 133 atom (13th CGPM, 1967).

Thermodynamic temperature: The unit of thermodynamic temperature called the *kelvin* is the fraction $1/273.16$ of the thermodynamic temperature of the triple point of water (13th CGPM, 1967).

Electric current: The unit of electric current called the *ampere* is that constant current which, if maintained in two straight parallel conductors of infinite length, of negligible circular cross-section, and placed 1 metre apart in a vacuum, would produce between these conductors a force equal to 2×10^{-7} newton per metre of length (9th CGPM, 1948).

Luminous intensity: The unit of luminous intensity called the *candela* is the luminous intensity, in a given direction, of a source that emits monochromatic radiation of frequency 540×10^{12} hertz and that has a radiant intensity in that direction of $(1/683)$ watt per steradian (16th CGPM, 1979).

Amount of substance: The *mole* is the amount of substance of a system which contains as many elementary entities as there are atoms in 0.012 kilogram of carbon 12 (14th CGPM, 1971).

Note: When the *mole* is used, the elementary entities must be specified and may be atoms, molecules, ions, electrons, other particles, or specified groups of such particles.

APPENDIX B

DEFINITIONS OF SOME DERIVED SI UNITS

Force: The unit of force called the *newton* is that force which, when applied to a body having a mass of 1 kilogram, gives it an acceleration of 1 metre per second per second. (Thus $1 \text{ N} = 1 \text{ kg m/s}^2$.)

Pressure: The unit of pressure called the *pascal** is equal to 1 newton per square metre. (Thus $1 \text{ Pa} = 1 \text{ N/m}^2$).

Energy: The unit of energy called the *joule* is the work done when the point of application of a force of 1 newton is displaced through a distance of 1 metre in the direction of the force. (Thus $1 \text{ J} = 1 \text{ N m}$.)

Power: The unit of power called the *watt* is equal to 1 joule per second.

Electric charge: The unit of electric charge called the *coulomb* is the quantity of electricity transported in 1 second by a current of 1 ampere.

Electric potential: The unit of electric potential called the *volt* is the difference of potential between two points of a conducting wire carrying a constant current of 1 ampere, when the power dissipated between these points is equal to 1 watt.

* This name for the N/m^2 is not used in these tables.

APPENDIX C

SI PREFIXES

Factor	Prefix	Symbol	Factor	Prefix	Symbol
10^{24}	yotta	Y	10^{-1}	deci	d
10^{21}	zetta	Z	10^{-2}	centi	c
10^{18}	exa	E	10^{-3}	milli	m
10^{15}	peta	P	10^{-6}	micro	μ
10^{12}	tera	T	10^{-9}	nano	n
10^9	giga	G	10^{-12}	pico	p
10^6	mega	M	10^{-15}	femto	f
10^3	kilo	k	10^{-18}	atto	a
10^2	hecto	h	10^{-21}	zehta	z
10^1	deca	da	10^{-24}	yocto	y

APPENDIX D

DEFINITIONS OF SOME NON-SI METRIC UNITS

Each equation serves to define **exactly** the unit appearing on the left-hand side of the equation.

Length:

1 micron	=	10^{-6} m	=	1 μm
1 ångström (Å)	=	10^{-10} m		

Volume: 1 litre (l) = 1000 cm³ = 1 dm³ = 10⁻³ m³

Note: This is the *litre* of the 12th CGPM, 1964. It is not identical to that previously defined by the 3rd CGPM, 1901, as the volume occupied by a mass of 1 kg of pure water at its temperature of maximum density and under a pressure of 1 standard atmosphere.

1 litre (1901) $\approx 1.000\,028 \times 10^{-3} \text{ m}^3$. (Up to 1976, the 1901 litre was used in the definition of the UK gallon. To the number of significant figures quoted in Appendix E, this redefinition involved no change in magnitude.)

Mass: 1 tonne, or metric ton (t) = 10^3 kg

Force:

1 dyne (dyn)	=	1 g cm/s ² = 10 ⁻⁵ N
1 kilogram force (kgf)	=	9.806 65 N

Note: This is that force which, when applied to a body having a mass of 1 kg, gives it an acceleration equal to the international standard acceleration of 9.80665 m/s^2 . In Germany, the *kilogram force* is also given the name *Kilopond* (kp).

Pressure, stress: $1 \text{ bar (bar)} = 10^5 \text{ N/m}^2$

1 std. atmosphere (atm) = 1.013 25 bar = 0.101 325 MN/m²

$$1 \text{ tech. atmosphere (at)} = 1 \text{ kgf/cm}^2 \\ = 0.980665 \text{ bar} = 0.00980665 \text{ MN/m}^2$$

Note: This unit is also sometimes given the unit symbol *ata*.

$$\begin{aligned} 1 \text{ torr} &= 1/760 \text{ atm} \approx 133.0 \text{ N/m}^2 \\ &\approx 1 \text{ mmHg to within 1 part in 7 million} \\ 1 \text{ mmHg} &= 13.5951 \times 9.80665 \text{ N/m}^2 \\ &\approx 133.0 \text{ N/m}^2 \end{aligned}$$

Note: This is the pressure that would be exerted by a 1 mm column of mercury of density 13.5951 g/cm^3 under a gravitational acceleration equal to the international standard acceleration of 9.80665 m/s^2 .

Energy: 1 erg = 1 dyn cm = 10^{-7} Nm = 10^{-7} J
1 calorie (cal) = 4.1868 J

Note: This is the *International Table calorie*, defined thus by the Fifth International Conference on the Properties of Steam, 1956.

1 thermochemical calorie = 4.184 J

Dynamic viscosity: 1 poise (P) = 1 g/cm s = 1 dyn s/cm²
= 0.1 kg/m s = 0.1 N s/m²

Kinematic viscosity: 1 stokes (St) $= 1 \text{ cm}^2/\text{s} = 10^{-4} \text{ m}^2/\text{s}$

APPENDIX E

BRITISH UNITS—DEFINITIONS AND CONVERSION FACTORS

DEFINITIONS OF SOME BASIC UNITS

Each equation serves to define **exactly** the unit appearing on the left-hand side of the equation.

Length:	1 yard (yd) = 0.9144 m
Mass:	1 pound (lb) = 0.453 592 37 kg
Force:	1 poundal (pdl) = 1 lb ft/s ²
	1 pound force (lbf) = $\frac{9.806\ 65}{0.3048}$ pdl (≈ 32.2 pdl)

Note: This is the force which, when applied to a body having a mass of 1 lb, gives it an acceleration equal to the international standard acceleration of 9.806 65 m/s².

Specific energy: 1 Btu/lb = 5/9 cal/g

Note: This equation serves to define the *British Thermal Unit* (Btu). The calorie is here the *International Table calorie* defined in Appendix D.

CONVERSION FACTORS FOR MECHANICAL UNITS

Quantity	British unit	Conversion factor	SI unit
Length	1 inch (in)	$= \frac{0.9144 \times 100}{36}$	cm
	1 foot (ft)	$= \frac{0.9144}{3}$	m
	1 mile (mile)	$= \frac{0.9144 \times 1760}{1000}$	km
	1 ounce (oz)	$= \frac{0.453\ 592\ 37 \times 1000}{16}$	g
Mass	1 pound (lb)	$= 0.453\ 592\ 37$	kg
	1 hundredweight (cwt)	$= 0.453\ 592\ 37 \times 112$	kg
	1 ton (ton)	$= 0.453\ 592\ 37 \times 2240$	kg
	(1 US short ton)	$= 0.453\ 592\ 37 \times 2000$	kg)
Force	1 poundal (pdl)	$= 0.453\ 592\ 37 \times 0.3048$	N
	1 ounce force (ozf)	$= \frac{0.453\ 592\ 37 \times 9.806\ 65}{16}$	N
	1 pound force (lbf)	$= 0.453\ 592\ 37 \times 9.806\ 65$	N
	1 ton force (tonf)	$= 0.453\ 592\ 37 \times 9.806\ 65 \times 2240$	kN
		≈ 2.54	
		$= 0.3048$	
		≈ 1.61	
		≈ 28.35	
		≈ 0.4536	
		≈ 50.8	
		≈ 1016	
		≈ 907	
		≈ 0.1383	
		≈ 0.278	
		≈ 4.45	
		≈ 9.96	

Volume	1 UK gallon (gal)*	$= 4.546\,091\,6$	≈ 4.546	dm ³
	* Redefined in 1976			
Specific volume	(1 US gallon	$= 231 \times (2.54)^3 \times 10^{-3}$	≈ 3.785	dm ³
	1 ft ³ /lb	$= \frac{(0.3048)^3}{0.453\,592\,37} \times 10^3$	≈ 62.43	dm ³ /kg
Pressure, stress	1 tonf/in ²	$= \frac{0.453\,592\,37 \times 9.806\,65}{10^3} \left(\frac{12}{0.3048} \right)^2 \times 2240$	≈ 15.44	MN/m ²
	1 lbf/in ²	$= \frac{0.453\,592\,37 \times 9.806\,65}{10^3} \left(\frac{12}{0.3048} \right)^2$	≈ 6.895	kN/m ²
	1 inHg*	$= 25.4 \times 13.5951 \times 9.806\,65 \times 10^{-3}$	≈ 3.39	kN/m ²
	1 ftH ₂ O*	$= 0.3048 \times 9.806\,65$	≈ 2.99	kN/m ²
	* <i>Note:</i> These are equal respectively to the pressures that would be exerted by a 1 in column of mercury of density 13.5951 g/cm ³ , and by a 1 ft column of water of density 1 g/cm ³ , under the international standard acceleration of 9.806 65 m/s ² .			
Dynamic viscosity	1 lb/ft s = 1 pdl s/ft ²	$= \frac{0.453\,592\,37}{0.3048}$	≈ 1.488	kg/m s N s/m ²
Kinematic viscosity	1 ft ² /s	$= (0.3048)^2$	≈ 0.0929	m ² /s
Energy	1 ft lbf	$= 0.3048 \times 0.453\,592\,37 \times 9.806\,65$	≈ 1.356	J
Power	1 horsepower (hp)	$= 550 \times 0.3048 \times 0.453\,592\,37 \times 9.806\,65$	≈ 746	W
Specific fuel consumption	1 lb/hp h	$= \frac{10^3}{550 \times 0.3048 \times 9.806\,65 \times 3600}$	≈ 0.169	kg/MJ

CONVERSION FACTORS FOR THERMAL UNITS

Energy	1 Btu	$= \frac{4.1868 \times 0.453\,592\,37}{1.8}$	≈ 1.055	kJ
	1 therm ($\equiv 10^5$ Btu)	$= \frac{4.1868 \times 0.453\,592\,37}{1.8} \times 10^2$	≈ 105.5	MJ
Specific energy	1 Btu/lb	$= \frac{4.1868}{1.8}$	$= 2.326$	kJ/kg
Sp. heat-capacity	1 Btu/lb R	$= 4.1868$	≈ 4.19	kJ/kg K
Sp. entropy	1 ft lbf/lb R	$= 0.3048 \times 9.806\,65 \times 1.8$	≈ 5.38	J/kg K
Gas constant	1 Btu/h ft R	$= \frac{4.1868 \times 0.453\,592\,37}{3.6 \times 0.3048}$	≈ 1.73	W/m K
Thermal conductivity	1 Btu/h ft ² R	$= \frac{4.1868 \times 0.453\,592\,37}{3.6 \times (0.3048)^2}$	≈ 5.68	W/m ² K
Heat transfer coefficient				

Note: R is here the *rankine* unit of *thermodynamic temperature*, here defined in terms of the *kelvin* by the relation 1 R = (1/1.8) K.

APPENDIX F

TEMPERATURE

Thermodynamic temperature

In constructing *thermodynamically consistent* tables of thermodynamic properties, use has to be made of equations such as $Tds = dh - vdp$, in which the symbol T refers to the *thermodynamic temperature* defined by the equation

$$\frac{T_1}{T_2} = \frac{Q_1}{Q_2},$$

where Q_1 and Q_2 are respectively the quantities of heat received by and rejected from a cyclic heat power plant operating *reversibly* between two thermal-energy reservoirs at temperatures T_1 and T_2 .

Zero thermodynamic temperature is that temperature to which, with T_1 at a fixed positive value, T_2 tends as Q_2 tends to zero. It is unattainable in practice, but this *absolute zero of temperature* nevertheless constitutes a definite, fixed level of temperature. (The unattainability of this absolute zero of temperature might appear to result from the fact that, if Q_2 were zero, the cyclic heat power plant would constitute a *perpetual motion machine of the second kind*, so that the Second Law would be contravened. The point is more subtle than this, however, and is discussed by A. B. Pippard in Chapter 5 of *Elements of Classical Thermodynamics*, Cambridge University Press, 1957.)

The kelvin unit of thermodynamic temperature

With *zero* thermodynamic temperature defined, it is only necessary to assign an arbitrary number of units to some other *temperature level* in order exactly to define the *unit* of thermodynamic temperature.

The kelvin unit of thermodynamic temperature, defined in 1954 and redefined in 1967, when it was given the title *kelvin* and the *unit symbol* K, is that obtained by assigning to the temperature level at the *triple point* of water a value of **273.16** kelvins, namely **273.16** K. The precise definition of this unit is given in Appendix A.

Note: Unfortunately, thermodynamic temperatures are frequently written as $T^\circ\text{K}$ instead of, as here, $T\text{ K}$.

Celsius temperature

By virtue of long-established habit, it is convenient in practice to use a truncated thermodynamic temperature called the *Celsius temperature*, defined by the relation

$$t = T - 273.15,$$

where t *Celsius* (written symbolically as $t^\circ\text{C}$) is the Celsius temperature at a thermodynamic temperature of T kelvins (namely $T\text{ K}$).

The convenience of this practice arises from the fact that the Celsius temperature at the *ice point* (the freezing point of air-saturated water at 1 atm) is then very nearly, though not exactly, 0°C .

Note: A thermodynamic temperature expressed in kelvins is commonly described as the *absolute temperature*, in order to distinguish it from the *Celsius temperature*. That usage is followed in the warning note given on those tables in which temperatures are listed in kelvins.

APPENDIX G

CONVERSION FACTORS FOR TEMPERATURE

In the British system of units, the unit of thermodynamic temperature, here given the name *rankine* and the unit symbol R, is defined in terms of the kelvin by the relation

$$1 \text{ R} = (1/1.8) \text{ K},$$

so that at a thermodynamic temperature of T_k kelvins (namely $T_k \text{ K}$) the thermodynamic temperature is T_r rankines (namely $T_r \text{ R}$), where

$$T_r = 1.8 T_k.$$

In the same way as it is convenient in practice to use a truncated thermodynamic temperature called the *Celsius temperature*, it is also convenient to use its counterpart in the British system of units, the *Fahrenheit temperature*, defined by the relation

$$t_F = T_r - 459.67,$$

where t_F *Fahrenheit* (written symbolically as $t_F^\circ\text{F}$) is the Fahrenheit temperature at a thermodynamic temperature of T_r rankines (namely $T_r \text{ R}$). In this way, the Fahrenheit temperature at the *ice point* is very nearly, though not exactly, 32°F .

At a Celsius temperature of $t_C^\circ\text{C}$, the Fahrenheit temperature, $t_F^\circ\text{F}$, is given by the relation

$$t_F = 1.8 t_C + 32,$$

or, more conveniently,

$$(t_F + 40) = 1.8 (t_C + 40).$$

Note: The nomenclature and symbology used in this Appendix in relation to British units have not been standardised. Thermodynamic (absolute) temperatures are frequently written as $T^\circ\text{R}$ instead of, as here, $T \text{ R}$.

Temperature differences are expressed in kelvins or rankines, for which the unit symbols are respectively K and R, so that the use of such symbols for temperature difference as *degK*, *degC*, *degR*, and *degF* is avoided.

APPENDIX H

PRINCIPAL SOURCES OF DATA

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Thermodynamic Tables in SI (metric) Units

(*Système International d'Unités*)

R. W. HAYWOOD

Engineering Laboratory, University of Cambridge

This book of thermodynamic tables for students is an enlarged version in SI units of Mr Haywood's previous book *Thermodynamic Tables and other data* published by Cambridge University Press in 1956. It contains twice as many tables and now includes an *Enthalpy-Entropy Diagram for Steam* and a *Pressure-Enthalpy Diagram for Refrigerant-12* (both compiled by Mr Haywood and Dr J. H. Mathewman) in a pocket at the back.

In addition to steam and refrigerant tables, the book includes a table of molar enthalpies of gases at low pressure, a series of thermochemical tables, tables giving thermodynamic properties of air at low temperatures (for use in gas liquefaction and refrigeration calculations at cryogenic temperatures) and tables of transport properties of various fluids. A number of appendices define all units used in the tables and give both exact and approximate conversion factors to British units and to some non-SI metric units.

For this third edition, Mr Haywood has made a major change in the table of equilibrium constants, to suit more generally accepted current practice. The change to natural logarithms, in place of logarithms to the base 10, results in a significant change to the numerical values, while a much smaller change to the numerical values results from expressing partial pressures in bars instead of atmospheres. The new values are everywhere numerically consistent with the values given in the second edition, and a simple formula is given by which the latter may be calculated from the new tabulated figures. Definitions of two of the basic SI units, the *metre* and the *candela*, have been updated in accordance with promulgations at more recent CGPMs.

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